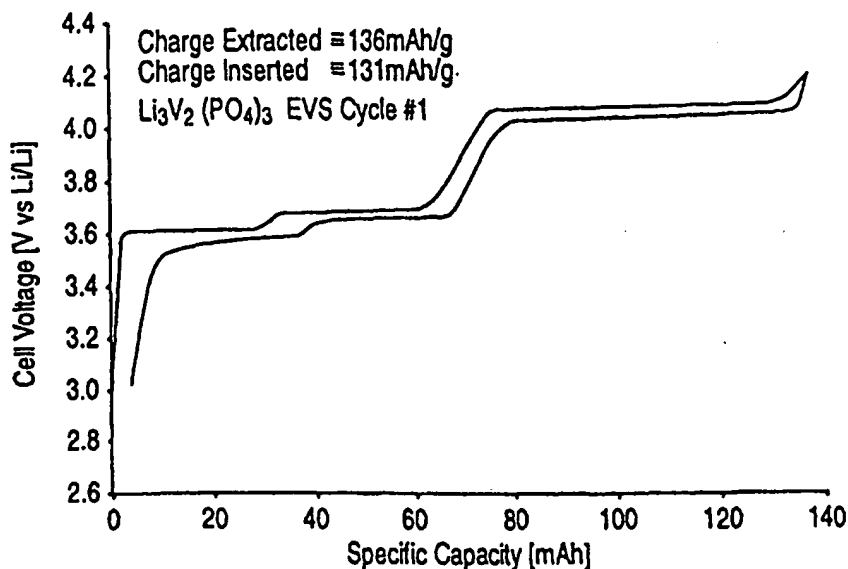


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INTERNATIONAL APPLICATION PUBLISHED UNDER THE PATENT COOPERATION TREATY (PCT)

(51) International Patent Classification 7 : H01M 4/58, 10/40, C01B 25/45		A1	(11) International Publication Number: WO 00/31812
			(43) International Publication Date: 2 June 2000 (02.06.00)
(21) International Application Number: PCT/US99/23074		(81) Designated States: AL, AM, AT, AU, AZ, BA, BB, BG, BR, BY, CA, CH, CN, CU, CZ, DE, DK, EE, ES, FI, GB, GE, GH, HU, IL, IS, JP, KE, KG, KP, KR, KZ, LC, LK, LR, LS, LT, LU, LV, MD, MG, MK, MN, MW, MX, NO, NZ, PL, PT, RO, RU, SD, SE, SG, SI, SK, SL, TJ, TM, TR, TT, UA, UG, US, UZ, VN, YU, ZW, ARIPO patent (GH, GM, KE, LS, MW, SD, SL, SZ, TZ, UG, ZW), Eurasian patent (AM, AZ, BY, KG, KZ, MD, RU, TJ, TM), European patent (AT, BE, CH, CY, DE, DK, ES, FI, FR, GB, GR, IE, IT, LU, MC, NL, PT, SE), OAPI patent (BF, BJ, CF, CG, CI, CM, GA, GN, GW, ML, MR, NE, SN, TD, TG).	
(22) International Filing Date: 5 October 1999 (05.10.99)			
(30) Priority Data: 09/195,961 19 November 1998 (19.11.98) US			
(63) Related by Continuation (CON) or Continuation-in-Part (CIP) to Earlier Application US 09/195,961 (CON) Filed on 19 November 1998 (19.11.98)			
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Published With international search report.			

(54) Title: LITHIUM BASED PHOSPHATES FOR USE IN LITHIUM ION BATTERIES AND METHOD OF PREPARATION



(57) Abstract

The invention provides an electrochemical cell which comprises an electrode having a lithium metal phosphorous compound.

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LITHIUM BASED PHOSPHATES FOR USE IN LITHIUM ION BATTERIES AND METHOD OF PREPARATION

5

Field of the Invention

10 This invention relates to improved materials usable as electrode active materials, method for making such improved materials, and electrodes formed from it for electrochemical cells in batteries.

Background of the Invention

15 Lithium batteries are prepared from one or more lithium electrochemical cells containing electrochemically active (electroactive) materials. Such cells typically include an anode (negative electrode), a cathode (positive electrode), and an electrolyte interposed between spaced
20 apart positive and negative electrodes. Batteries with anodes of metallic lithium and containing metal chalcogenide cathode active material are known. The electrolyte typically comprises a salt of lithium dissolved in one or more solvents, typically nonaqueous (aprotic)
25 organic solvents. Other electrolytes are solid electrolytes typically called polymeric matrixes that contain an ionic conductive medium, typically a metallic powder or salt, in combination with a polymer that itself may be ionically conductive which is electrically
30 insulating. By convention, during discharge of the cell, the negative electrode of the cell is defined as the anode. Cells having a metallic lithium anode and metal chalcogenide cathode are charged in an initial condition. During discharge, lithium ions from the metallic anode pass
35 through the liquid electrolyte to the electrochemical

active (electroactive) material of the cathode whereupon they release electrical energy to an external circuit.

It has recently been suggested to replace the lithium metal anode with an intercalation anode, such as a lithium metal chalcogenide or lithium metal oxide. Carbon anodes, such as coke and graphite, are also intercalation materials. Such negative electrodes are used with lithium-containing intercalation cathodes, in order to form an electroactive couple in a cell. Such cells, in an initial condition, are not charged. In order to be used to deliver electrochemical energy, such cells must be charged in order to transfer lithium to the anode from the lithium-containing cathode. During discharge the lithium is transferred from the anode back to the cathode. During a subsequent recharge, the lithium is transferred back to the anode where it reintercalates. Upon subsequent charge and discharge, the lithium ions (Li^+) are transported between the electrodes. Such rechargeable batteries, having no free metallic species are called rechargeable ion batteries or rocking chair batteries. See U.S. Patent Numbers 5,418,090; 4,464,447; 4,194,062; and 5,130,211.

Preferred positive electrode active materials include LiCoO_2 , LiMn_2O_4 , and LiNiO_2 . The cobalt compounds are relatively expensive and the nickel compounds are difficult to synthesize. A relatively economical positive electrode is LiMn_2O_4 , for which methods of synthesis are known, and involve reacting generally stoichiometric quantities of a lithium-containing compound and a manganese containing compound. The lithium cobalt oxide (LiCoO_2), the lithium manganese oxide (LiMn_2O_4), and the lithium nickel oxide (LiNiO_2) all have a common disadvantage in that the charge capacity of a cell comprising such cathodes suffers a significant loss in capacity. That is, the initial capacity available (amp hours/gram) from LiMn_2O_4 , LiNiO_2 , and LiCoO_2 is less than the theoretical capacity because less than 1 atomic unit of lithium engages in the

electrochemical reaction. Such an initial capacity value is significantly diminished during the first cycle operation and such capacity further diminishes on every successive cycle of operation. The specific capacity for LiMn_2O_4 is at best 148 milliamp hours per gram. As described by those skilled in the field, the best that one might hope for is a reversible capacity of the order of 110 to 120 milliamp hours per gram. Obviously, there is a tremendous difference between the theoretical capacity (assuming all lithium is extracted from LiMn_2O_4) and the actual capacity when only 0.8 atomic units of lithium are extracted as observed during operation of a cell. For LiNiO_2 and LiCoO_2 , only about 0.5 atomic units of lithium is reversibly cycled during cell operation. Many attempts have been made to reduce capacity fading, for example, as described in U.S. Patent No. 4,828,834 by Nagaura et al. However, the presently known and commonly used, alkali transition metal oxide compounds suffer from relatively low capacity. Therefore, there remains the difficulty of obtaining a lithium-containing chalcogenide electrode material having acceptable capacity without disadvantage of significant capacity loss when used in a cell.

Summary of the Invention

The invention provides novel lithium-containing phosphate materials having a high proportion of lithium per formula unit of the material. Upon electrochemical interaction, such material deintercalates lithium ions, and is capable of reversibly cycling lithium ions. The invention provides a rechargeable lithium battery which comprises an electrode formed from the novel lithium-containing phosphates, preferably lithium-metal-phosphates. Methods for making the novel phosphates and methods for using such phosphates in electrochemical cells are also provided. Accordingly, the invention provides a rechargeable lithium battery which comprises an electrolyte; a first electrode having a compatible active material; and a second electrode comprising the novel phosphate materials. The novel materials, preferably used as a positive electrode active material, reversibly cycle lithium ions with the compatible negative electrode active material. Desirably, the phosphate has a proportion in excess of 2 atomic units of lithium per formula unit of the phosphate, and upon electrochemical interaction the proportion of lithium ions per formula unit become less. Desirably, the lithium-containing phosphate is represented by the nominal general formula $\text{Li}_a\text{E}'_b\text{E}''_c(\text{PO}_4)$, where in an initial condition "a" is about 3, and during cycling varies as $0 \leq a \leq 3$; b and c are both greater than 0, and b plus c is about 2. In one embodiment, elements E' and E'' are the same. In another embodiment, E' and E'' are different from one another. At least one of E' and E'' is an element capable of an oxidation state higher than that initially present in the lithium phosphate compound. Correspondingly, at least one of E' and E'' has more than one oxidation state. Both E' and E'' may have more than one oxidation state and both may be oxidizable from the state initially present in the phosphate compound. Desirably, at least one

of E' and E" is a metal or semi-metal. Preferably, at least one of E' and E" is a metal. Preferably, the phosphate is represented by the nominal general formula $\text{Li}_3\text{M}'_b\text{M}''_c(\text{PO}_4)_3$, where M' and M" are each metalloids or metals, b plus c is about 2, and M' and M" satisfy the conditions of oxidizability and oxidation state given for E' and E". Many combinations satisfying the above conditions are possible. For example, in one embodiment M' and M" are each transition metals. In still another embodiment of the formulation $\text{Li}_3\text{M}'_y\text{M}''_{2-y}(\text{PO}_4)_3$, M' may be selected from non-transition metals and semi-metals (metalloids). In another embodiment, such non-transition metal has only one oxidation state and is nonoxidizable from its oxidation state in the final compound $\text{Li}_3\text{M}'_y\text{M}''_{2-y}(\text{PO}_4)_3$. In this case, M' may be selected from metals, such as aluminum, magnesium, calcium, potassium, and other Groups I and II metals. In this case, M" has more than one oxidation state, and is oxidizable from its oxidation state in the end product, and M" is preferably a transition metal. In another embodiment, the non-transition-metal element has more than one oxidation state. In one preferred embodiment, M" is a transition metal, and M' is a non-transition-metal metal. Here, M' may be Mg, Be, Ca, Sn, Pb, Ge, B, K, Al, Ga, In, As or Sb; and M" may be Ti, V, Cr, Mn, Fe, Co, Ni, Cu, Mo, W, Zn, Cd or Pd. For example, M' is +3 and M" is +3 oxidation state. These oxidation states are merely exemplary, as many combinations are possible. In still another preferred embodiment, one metal is Zr or Ti, and the other metal is a metal characterized by a +2 oxidation state. Here, M⁺² may be Ti, V, Cr, Mn, Fe, Co, Ni, Cu, Sn, Pb, Mo, W, Zn, Cd or Pd. The Zr and Ti each have +4 oxidation state.

Examples of semi-metals having more than one oxidation state are selenium and tellurium; other non-transition metals with more than one oxidation state are tin and lead. Metallic elements include metals and semi-

metals, such as semi-conductors, including silicon (Si), tellurium (Te), selenium (Se), antimony (Sb), and arsenic (As).

Among the metals and metalloids useful as M', M" or both, there are B (Boron), Ge (Germanium), As (Arsenic), Sb (Antimony), Si (Silicon), and Te (Tellurium). The selenium and sulfur elements are also able to form positive ions but are less desirable. Among the useful metals which are not transition metals, there are the Group IA (New IUPAC 1) alkali; the Group IIA (New IUPAC 2) alkaline; the Group IIIA (13); the Group IVA (14); and the Group VA (15). The useful metals which are transition metals are Groups IIIB (3) to IIB (12), inclusive. Particularly useful are the first transition series transition metals of the 4th Period of the Periodic Table. The other useful transition metals are found in the 5th and 6th Periods, and a few in the 7th Period. Among the useful metals which are not transition metals, there are the Group IA (New IUPAC 1) alkali, particularly Li (Lithium), Na (Sodium), K (Potassium), Rb (Rubidium), Cs (Caesium); the Group IIA (New IUPAC 2) alkaline, particularly Be (Beryllium), Mg (Magnesium), Ca (Calcium), Sr (Strontium), Ba (Barium); the Group IIIA (13) Al (Aluminum), Ga (Gallium), In (Indium), Tl (Thallium); the Group IVA (14) Sn (Tin), Pb (Lead); and the Group VA (15) Bi (Bismuth). The useful metals which are transition metals are Groups IIIB (3) to IIB (12), inclusive. Particularly useful are the first transition series (4th Period of the Periodic Table), Sc (Scandium), Ti (Titanium), V (Vanadium), Cr (Chromium), Mn (Manganese), Fe (Iron), Co (Cobalt), Ni (Nickel), Cu (Copper), Zn (Zinc). The other useful transition metals are Y (Yttrium), Zr (Zirconium), Nb (Niobium), Mo (Molybdenum), Ru (Ruthenium), Rh (Rhodium), Pd (Palladium), Ag (Silver), Cd (Cadmium), Hf (Hafnium), Ta (Tantalum), W (Tungsten), Re (Rhenium), Os (Osmium), Ir (Iridium), Pt (Platinum), Au (Gold), Hg

(Mercury); and the lanthanides, particularly La (Lanthanum), Ce (Cerium), Pr (Praseodymium), Nd (Neodymium), Sm (Samarium). M is most desirably a first transition series transition metal, Sc, Ti, V, Cr, Mn, Fe, Co, Ni, Cu, Zn; other desirable transition metals are Zr, Mo, and W. Mixtures of transition metals are also desirable.

The phosphates are alternatively represented by the nominal general formula $\text{Li}_{3-x}\text{M}'_y\text{M}''_{2-y}(\text{PO}_4)_3$ ($0 \leq x \leq 3$), signifying capability to deintercalate and reinsert lithium. $\text{Li}_{3-x}\text{M}'_y\text{M}''_{2-y}(\text{PO}_4)_3$ signifies that the relative amount of M' and M'' may vary, with $0 \leq y \leq 2$, preferably, some M' and M'' are each present. The same criteria as to the values of x and y apply to $\text{Li}_{3-x}\text{E}'_y\text{E}''_{2-y}(\text{PO}_4)_3$. The active material of the counter electrode is any material compatible with the lithium-metal-phosphate of the invention. Where the lithium-metal-phosphate is used as a positive electrode active material, metallic lithium may be used as the negative electrode active material where lithium is removed and added to the metallic negative electrode during use of the cell. The negative electrode is desirably a nonmetallic intercalation compound. Desirably, the negative electrode comprises an active material from the group consisting of metal oxide, particularly transition metal oxide, metal chalcogenide, carbon, graphite, and mixtures thereof. It is preferred that the anode active material comprises graphite. The lithium-metal-phosphate of the invention may also be used as a negative electrode material.

The present invention resolves the capacity problem posed by widely used cathode active material. It has been found that the capacity of cells having the preferred $\text{Li}_3\text{M}'\text{M}''(\text{PO}_4)_3$ active material of the invention are greatly improved, for example, over LiMn_2O_4 . Optimized cells containing lithium-metal-phosphates of the invention potentially have performance greatly improved over all of

the presently used lithium metal oxide compounds. Advantageously, the novel lithium-metal-phosphate compounds of the invention are relatively easy to make, and readily adaptable to commercial production, are relatively low in cost, and have very good specific capacity.

Objects, features, and advantages of the invention include an improved electrochemical cell or battery based on lithium which has improved charging and discharging characteristics, a large discharge capacity, and which maintains its integrity during cycling. Another object is to provide a cathode active material which combines the advantages of large discharge capacity and with relatively lesser capacity fading. It is also an object of the present invention to provide positive electrodes which can be manufactured more economically and relatively more conveniently, rapidly, and safely than present positive electrodes which react readily with air and moisture. Another object is to provide a method for forming cathode active material which lends itself to commercial scale production providing for ease of preparing large quantities.

These and other objects, features, and advantages will become apparent from the following description of the preferred embodiments, claims, and accompanying drawings.

Brief Description of the Drawings

Figure 1 is an EVS (Electrochemical Voltage Spectroscopy) voltage/capacity profile for a cell embodying the lithium-metal-phosphate material of the invention $\text{Li}_3\text{V}_2(\text{PO}_4)_3$ in combination with a lithium metal counter electrode in an electrolyte comprising ethylene carbonate (EC) and dimethyl carbonate (DMC) in a weight ratio of 2:1 and including a 1 molar concentration of LiPF_6 salt. The lithium-metal-phosphate containing electrode and the lithium metal counter electrode are maintained spaced apart by a separator of fiber glass which is interpenetrated by the solvent and the salt. The conditions are ± 10 mV steps, between about 3.0 and 4.2 volts, and the critical limiting current density is less than or equal to 0.05 mA/cm^2 .

Figure 2 is an EVS differential capacity plot for the cell as described in connection with Figure 1.

Figure 3 is a voltage/capacity plot of $\text{Li}_3\text{V}_2(\text{PO}_4)_3$ cycled with a lithium metal anode using constant current cycling at ± 0.2 milliamps per square centimeter in a range of 3.0 to 4.3 volts.

Figure 4 is a two-part graph based on multiple constant current cycling of $\text{Li}_3\text{V}_2(\text{PO}_4)_3$ cycled with a lithium metal anode using the electrolyte as described in connection with Figure 1 and cycled, charge and discharge at ± 0.25 milliamps per square centimeter, 3.0 to 4.2 volts. In the two-part graph, Figure 4A shows the excellent rechargability of the lithium-metal-phosphate/lithium metal cell. Figure 4B shows the excellent cycling and capacity of the cell.

Figure 5 is an illustration of a cross section of a thin battery or cell embodying the invention.

Figure 6 shows the results of an x-ray diffraction analysis of the $\text{Li}_3\text{V}_2(\text{PO}_4)_3$, prepared according to the invention using $\text{CuK}\alpha$ radiation, $\lambda = 1.5418 \text{ \AA}$.

5 Figure 7 is an EVS voltage/capacity profile for a cell containing $\text{Li}_3\text{AlV}(\text{PO}_4)_3$, positive electrode of the invention in combination with a lithium metal counter-electrode in an electrolyte as described with respect to Figure 1 above. The conditions of the test are as described with respect to Figure 1 above.

10 Figure 8 is an EVS differential capacity plot for the cell as described in connection with Figure 7.

Figure 9 shows the results of the first constant current cycling at plus/minus 0.05 milliamps per square centimeter between about 3 and 4.5 volts based on the $\text{Li}_{3-x}\text{AlV}(\text{PO}_4)_3$, active material in the cathode.

15 Figure 10 is a graph based on multiple constant current cycling at plus/minus 0.05 milliamps per square centimeter versus metallic lithium counter-electrode.

Figure 11 is a voltage/capacity plot of $\text{Li}_3\text{V}_2(\text{PO}_4)_3$, cycled with a carbon-based negative electrode using constant current cycling at plus/minus 0.2 milliamps per square centimeter in a range of 2.5 to 4.1 volts.

20 Figure 12 presents data obtained by multiple current cycling at about plus/minus 0.2 milliamps per square centimeter between about 2.5 to 4.1 volts.

Figure 13 is an EVS voltage/capacity profile for a cell containing $\text{Li}_3\text{AlV}(\text{PO}_4)_3$, positive electrode made under H_2 atmosphere cycled with a lithium metal counter-electrode in an electrolyte. The cell is as described with respect to Figure 1 above. The conditions of the test are also as described with respect to Figure 1 above.

30 Figure 14 is an EVS differential capacity plot for the cell as described in connection with Figure 13.

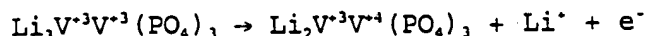
Figure 15 shows the results of the first constant current cycling at plus/minus 0.05 milliamps per square centimeter between about 3 and 4.2 volts based on the

$\text{Li}_{3-x}\text{AlV}(\text{PO}_4)_3$, active material in the cathode prepared under H_2 atmosphere.

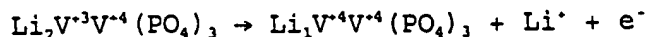
Detailed Description of the
Preferred Embodiments

The present invention provides lithium-containing
5 phosphate materials, preferably lithium-metal-phosphates,
which are usable as electrode active materials, for
the first time, as a source of lithium (Li^+) ions.
Upon extraction of x lithium ions from the preferred
10 $\text{Li}_{3-x}\text{M}'\text{M}''(\text{PO}_4)_3$, significant capacity is achieved. Such
specific capacity achieved from preferred lithium-metal-
phosphates is far in excess of the specific capacity from
 $\text{Li}_1\text{Mn}_2\text{O}_4$ ($\text{Li}_{1-x}\text{Mn}_2\text{O}_4$), an example of a currently used cathode
active material. In the method of the invention,
15 electrochemical energy is provided by deintercalation of
lithium from lithium-metal-phosphates ($\text{Li}_3\text{M}'\text{M}''(\text{PO}_4)_3$). For
example, when lithium is removed per formula unit of the
 $\text{Li}_3\text{M}'\text{M}''(\text{PO}_4)_3$, vanadium is oxidized from vanadium III to
vanadium IV or V in $\text{Li}_3\text{M}_2(\text{PO}_4)_3$, $\text{M}_2 = \text{V}_2$.

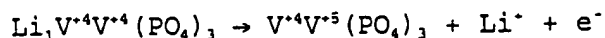
When 1 lithium is removed per formula unit of the
20 lithium vanadium phosphate, V^{III} is oxidized to V^{IV} . The
electrochemical reaction is as shown below:



25 Further extraction is possible according to:



Note that the average oxidation state of vanadium is +4
30 (IV). It is thought that both of the vanadium atomic
species carry a +4 charge, it is less likely that one of
the vanadium species carries a +3 charge and the other a +5
charge. Advantageously, still further oxidation is
possible with the removal of the final lithium ion
35 according to the Equation:



In the overall equation $\text{Li}_3\text{V}^{3+}\text{V}^{5+}(\text{PO}_4)_3 \rightarrow \text{V}^{4+}\text{V}^{5+}(\text{PO}_4)_3 + 3\text{Li}^+ + 3\text{e}^-$, this material has a theoretical capacity of 197 milliamp hours per gram upon electrochemical oxidation as per the reaction shown herein. The electrochemical extraction of lithium from $\text{Li}_3\text{M}'\text{M}''(\text{PO}_4)_3$ is heretofore not known to have been described. Similarly, a mixed metal compound, such as $\text{Li}_3\text{FeV}(\text{PO}_4)_3$, has two oxidizable elements. In contrast, $\text{Li}_3\text{AlTm}(\text{PO}_4)_3$ has one oxidizable metal, the transition metal (Tm).

Figures 1 through 4 which will be described more particularly below shows capacity in actual use where the lithium-metal-phosphate cathode (positive electrode) of the invention was tested in a cell comprising a lithium metal counter electrode (negative electrode) and an EC:DMC-LiPF₆ electrolyte, with operation between about 3.0 and 5.0 volts versus L/Li⁺ where lithium is cycled between the positive electrode and the negative electrode.

In another aspect, the invention provides a lithium ion battery which comprises an electrolyte; a negative electrode having an intercalation active material; and a positive electrode comprising a lithium-metal-phosphate active material characterized by an ability to deintercalate lithium ions for intercalation into the negative electrode active material. The lithium-metal-phosphate is desirably represented by the nominal general formula $\text{Li}_3\text{M}'\text{M}''(\text{PO}_4)_3$. In one aspect, the metals M' and M'' are the same and in another aspect, the metals M' and M'' are different. Desirably, the phosphate is the compound $\text{Li}_3\text{M}_2(\text{PO}_4)_3$, where M is a transition metal, and M is most desirably V, Fe, Cr, Ni, Co, and Mn. The lithium-metal-phosphate is preferably a compound represented by the nominal general formula $\text{Li}_{3-x}\text{V}_2(\text{PO}_4)_3$, signifying the preferred composition and its capability to deintercalate lithium. The present invention resolves a capacity problem

posed by conventional cathode active materials. Such problems with conventional active materials are described by Tarascon in U.S. Patent No. 5,425,932, using LiMn_2O_4 as an example. Similar problems are observed with LiCoO_2 , LiNiO_2 , and many, if not all, lithium metal chalcogenide materials. The present invention demonstrates that such capacity problems are overcome and greater proportion of available capacity in the cathode active material is utilizable providing a great improvement over conventional active materials.

The positive electrode active material in an initial condition is represented by the molecular formula $\text{Li}_{1-x}\text{M}'\text{M}''(\text{PO}_4)_3$. When used in a cell it deintercalates a quantity of x lithium ions for intercalation into the negative electrode, where the amount of x ions deintercalated is greater than 0 and less than or equal to 3. Accordingly, during cycling, charge and discharge, the value of x varies as x greater than or equal to 0 and less than or equal to 3.

Positive electrode lithium-metal-phosphate active material was prepared and tested in electrochemical cells and the results are reported in Figures 1 through 4. A typical cell configuration will be described with reference to Figure 5.

A description of the electrochemical cell or battery which uses the novel active material of the invention will now be described. By convention, an electrochemical cell comprises a first electrode, a counter electrode which reacts electrochemically with the first electrode, and an electrolyte which is capable of transferring ions between the electrodes. A battery refers to one or more electrochemical cells. Referring to Figure 5, an electrochemical cell or battery 10 has a negative electrode side 12, a positive electrode side 14, and an electrolyte/separator 16 therebetween. The negative electrode is the anode during discharge, and the positive

electrode is the cathode during discharge. The negative electrode side includes current collector 18, typically of nickel, iron, stainless steel, and copper foil, and negative electrode active material 20. The positive electrode side includes current collector 22, typically of aluminum, nickel, and stainless steel, and such foils may have a protective conducting coating foil, and a positive electrode active material 24. The electrolyte/separator 16 is typically a solid electrolyte, or separator and liquid electrolyte. Solid electrolytes typically referred to as polymeric matrixes which contain an ionic conductive medium. Liquid electrolytes typically comprise a solvent and an alkali metal salt which form an ionically conducting liquid. In this latter case, the separation between the anode and cathode is maintained, for example, by a relatively inert layer of material such as glass fiber. The electrolyte is not an essential feature of the invention. Essentially, any lithium ion containing conducting electrolyte may be used, that is stable up to 4.5 volts or more. Essentially any method may be used to maintain the positive and negative electrodes spaced apart and electrically insulated from one another in the cell. Accordingly, the essential features of the cell are the positive electrode, a negative electrode electrically insulated from the positive electrode, and an ionically conducting medium between the positive and negative electrodes. Examples of a suitable separator/electrolyte, solvents, and salts are described in U.S. Patent No. 4,830,939 showing a solid matrix containing an ionically conducting liquid with an alkali metal salt where the liquid is an aprotic polar solvent; and U.S. Patent Numbers 4,935,317; 4,990,413; 4,792,504; and 5,037,712. Each of the above patents is incorporated herein by reference in its entirety.

Electrodes of the invention are made by mixing a binder, the active material, and carbon powder (particles

of carbon). The binder desirably is a polymer. A paste containing the binder, active material, and carbon, is coated onto a current collector.

5 Positive Electrode

A positive electrode containing the lithium phosphate compound, preferably lithium-metal-phosphate, active material of the invention is prepared by the following method. For the positive electrode, the content
10 was as follows: 50 to 90 percent by weight active material ($\text{Li}_3\text{M}'\text{M}''(\text{PO}_4)_3$); 5 to 30 percent carbon black as the electrically conductive diluent; and 3 to 20 percent binder. The stated ranges are not critical. The amount of active material may range from 25 to 85 weight percent. The
15 formation of each electrode will now be described. The positive electrode was prepared from mixtures of lithium-metal-phosphate (active material) and EPDM (ethylene propylene diene monomer) as the binder, Shawinigan Black® was used as the carbon powder conductive diluent. The
20 carbon powder conductive diluent is used to enhance electronic conductivity of the lithium-metal-phosphate. Shawinigan Black®, available from Chevron Chemical Company, San Ramone, California, has a BET average surface area of about 70 ± 5 square meters per gram. Other suitable carbon
25 blacks are sold under the designation Super P™ and Super S™ available from MMM, a subsidiary of Sedema, which carbons have BET surface areas of about 65 ± 5 square meters per gram. (MMM has its headquarters in Brussels, Belgium.) Examples of suitable polymeric binders include EPDM
30 (ethylene propylene diene termonomers), PVDF (polyvinylidene difluoride), ethylene acrylic acid copolymer, EVA (ethylene vinyl acetate copolymer), copolymer mixtures, and the like. It is desirable to use either PVDF available from Polysciences Corporation with a
35 molecular weight of 120,000 or EPDM available from Exxon Corporation and sold under the designation EPDM 2504™. EPDM

is also available from The Aldrich Chemical Company. The description of carbon powders and binders constitute representative examples and the invention is not limited thereby. For example, other carbon powders are available from Exxon Chemicals, Inc., Chicago, Illinois under the trade name Ketjen Black EC 600 JD[®] and polyacrylic acid of average molecular weight 240,000 is commercially available from BF Goodrich, Cleveland, Ohio under the name Good-Rite K702[™]. The positive electrodes of the invention comprised mixtures of the lithium-metal-phosphate active material, the binder (EPDM), and the carbon particles (Shawinigan Black[®]). These were mixed and blended together with a solvent. Xylene is a suitable solvent. The mixture was then coated onto an aluminum foil current collector to achieve a desired thickness for the final electrode.

Electrolyte

The electrolyte used to form the completed cell is preferably a combination of EC/DMC when a carbon counter electrode is used. That is, ethylene carbonate (EC) and dimethyl carbonate (DMC). The ratio of EC:DMC was about 2:1 by weight. Generally, when a lithium metal anode is used, the choice of an electrolyte is less restricted. It may be the EC:DMC in a ratio of 2:1 by weight or, for example, EC:PC (propylene carbonate) in 50:50 by weight ratio. In any case, the preferred salt is 1 molar LiPF₆. Positive and negative electrodes are maintained in a separated condition using a fiber glass layer. Such separation can also be achieved using a layer of Celgard[™]. Hoechst - Celanese Corp., Celgard 2400[™], porous polypropylene, 25 microns thick.

Negative Electrode

The electrochemical cell used with the positive electrode and electrolyte may contain one of a variety of negative electrode active materials. In one embodiment,

the negative electrode may be metallic lithium. In more desirable embodiments, the negative electrode is an intercalation active material, such as, metal oxides and graphite. When a metal oxide active material is used, the components of the electrode are the metal oxide, electrically conductive carbon black, and binder in the proportions as described above for the positive electrode. Representative, but not limiting, examples include coke, graphite, WO_3 , Nb_2O_5 , and V_6O_{11} . In a preferred embodiment, the negative electrode active material is graphite particles. For test purposes, for determining capacity of a positive electrode, test cells were fabricated using the lithium metal active material. When test cells are formed such as to be used as batteries, a nonmetallic intercalation graphite electrode is preferred. The preferred graphite-based negative electrode comprises about 80 to 95 percent by weight graphite particles, and more preferably about 90 percent by weight with the balance constituted by a binder. Preferably, the anode is prepared from a graphite slurry as follows. A polyvinylidene difluoride (PVDF) solution is prepared by mixing 300 grams of 120,000 MW PVDF (PolyScience) in 300 ml of dimethyl formamide. The mixture was stirred for 2 to 3 hours with a magnetic stirrer to dissolve all of the PVDF. The PVDF functions as a binder for the graphite in the anode. Next, a PVDF/graphite slurry is prepared by first adding 36 grams of graphite (SFG-15) into about 38.5 grams of the PVDF solution. The mixture is homogenized with a commercial homogenizer or blender. (For example, Tissue Homogenizer System from Cole-Parmer Instrument Co., Niles, IL). The viscosity of the slurry is adjusted to about 200 cp with additional PVDF solution. The slurry is coated onto a bare copper foil by standard solvent casting techniques, such as by a doctor blade type coating. (Alternatively, the slurry can be coated onto a copper foil having a polymeric adhesion promoter layer, described above.) In preparing the

slurry, it is not necessary to grind or dry the graphite, nor is it necessary to add conductive carbon black to the graphite anode formulation. Finally, the electrodes are dried at approximately 150°C for 10 hours to remove residual water prior to making the electrochemical cells.

In one embodiment, the negative electrode has the lithium-metal-phosphate compound as the active material. In the case of $\text{Li}_3\text{V}^{3+}\text{V}^{3+}(\text{PO}_4)_3$, the V^{3+} would theoretically be reduced to V^{2+} . For $\text{Li}_3\text{Fe}^{3+}\text{Fe}^{3+}(\text{PO}_4)_3$, the same activity is theoretically possible, since Fe^{2+} is a stable and common oxidation state for Fe. This should allow two more lithium ions to be inserted. That is, $\text{Li}_{3+x}\text{Fe}_2(\text{PO}_4)_3$, x is about 2.

Various methods for fabricating electrochemical cells and for forming electrode components are described herein. The invention is not, however, limited by any particular fabrication method as the novelty lies in the unique positive electrode material itself and combination of positive and negative electrode materials. Examples of forming cells containing a variety of electrodes and electrolytes can be found in U.S. Patent Nos. 4,668,595; 4,830,939; 4,935,317; 4,990,413; 4,792,504; 5,037,712; 5,262,253; 5,300,373; 5,435,054; 5,463,179; 5,399,447; 5,482,795 and 5,411,820; each of which is incorporated herein by reference in its entirety. Note that the older generation of cells contained organic polymeric and inorganic electrolyte matrix materials, with the polymeric being most preferred. The polyethylene oxide of 5,411,820 is an example. More modern examples are the VDF:HFP polymeric matrix. Examples of casting, lamination and formation of cells using VdF:HFP are as described in U.S. Patent Nos. 5,418,091; 5,460,904; 5,456,000; and 5,540,741; assigned to Bell Communications Research, each of which is incorporated herein by reference in its entirety.

The compositions of the invention are prepared by mixing together appropriate proportions of precursor compounds. In one preferred embodiment, precursor

compounds are in powder form, mixtures of such powders are intermingled and then heated at a temperature sufficient to cause formation of the desired lithium-phosphates of the invention. In this example, the compositions of the invention are prepared by mixing together appropriate proportions of: alkali metal carbonate, here lithium metal carbonate (Li_2CO_3); a phosphoric acid derivative, preferably the phosphoric acid ammonium acid salt, ammonium phosphate, $\text{NH}_4\text{H}_2(\text{PO}_4)$ or $(\text{NH}_4)_2\text{H}(\text{PO}_4)$; and selected metal salts and metal oxides, preferably, MO_x , $0 < x \leq 3$; phosphates, nitrates and acetates. Examples are, MgO , $\text{Mg}_3(\text{PO}_4)_2$, $\text{Mg}(\text{NO}_3)_2$, MnO , MnO_2 , Mn_2O_3 , MoO_2 , MoO_3 , FeO , Fe_2O_3 , Cr_2O_3 , ZrO_2 , NiO , CoO , VO , V_2O_3 , V_2O_5 , CuO , TiO , TiO_2 , LiAlO_2 , AlOH , Al_2O_3 , AlPO_4 , B_2O_3 , BPO_4 , K_2O , SnO , SnO_2 , PbO , PbO_2 , $\text{Ga}(\text{NO}_3)_3$, Ga_2O_3 , In_2O_3 , $\text{In}(\text{NO}_3)_3$, As_2O_3 , Sb_2O_3 , BeO , CaO , $\text{Ca}_3(\text{PO}_4)_2$, $\text{Ca}(\text{NO}_3)_2$, GeO_2 , zinc acetate, ZnO , $\text{Zn}(\text{NO}_3)_2$, CdO and $\text{Cd}(\text{NO}_3)_2$. The selection of precursor in part depends on whether a reducing, inert or ambient atmosphere is used.

In one embodiment, in order to obtain compositions of the compound $\text{Li}_3\text{V}_2(\text{PO}_4)_3$, appropriate mixtures of Li_2CO_3 ; V_2O_5 or V_2O_3 ; and $\text{NH}_4\text{H}_2\text{PO}_4$ are used. The proportions are on the basis of molar ratios. The mixture is heated for a number of hours, and at a temperature sufficient to decompose the phosphate. Then the mixture is held at an elevated temperature of about 700°C to about 950°C for several hours. Repeated cooling, grinding and reheating at an elevated temperature may be necessary in order to cause complete reaction to form the final product.

In another embodiment, a product of the nominal general formula $\text{Li}_3\text{AlV}(\text{PO}_4)_3$ is prepared by mixing appropriate amounts of Li_2CO_3 ; $\text{Al}(\text{OH})_3$ or Al_2O_3 ; V_2O_5 or V_2O_3 ; and $\text{NH}_4\text{H}_2\text{PO}_4$. The relative molar proportions are selected based on the atomic amounts of each component in the final product. Those skilled in the art will also recognize that preparation by the sol-gel is advantageous, facilitating cycling since the compound is not as crystal-like.

Amorphous materials often provide plateaus on cycling that are less defined. NASICON phases are commonly known in rhombohedral or monoclinic structure. Some exist in more than one form. The form of the product depends on the method of preparation. Therefore, the degree of crystallinity changes, depending on particle size and process parameters.

The Examples below show methods of preparing compounds of the nominal general formula $\text{Li}_3\text{M}'\text{M}''(\text{PO}_4)_3$. The method comprises providing a lithium-containing compound, one or more metal oxide compounds, and a phosphoric acid containing compound. Preferably, the lithium-containing compound is a lithium salt and the phosphoric acid compound is a phosphoric acid salt. The lithium compound, one or more metal or metalloid compounds, and phosphoric acid based compound are mixed together in a proportion which provides the stated nominal general formula. Such precursor compounds are intimately mixed and then reacted together where the reaction is initiated by heat and is desirably conducted in a nonoxidizing, preferably reducing atmosphere, whereby the lithium, M from the metal/metalloid compound (oxide) and phosphate combine to form the $\text{Li}_3\text{M}'\text{M}''(\text{PO}_4)_3$. The temperatures required to decompose precursor(s), initiate reaction and then complete the reaction depend, in part, on the precursors. A first heating is at a first temperature of about 550°C to about 750°C, and a second heating is at a second temperature of about 800°C to about 1000°C. Before reacting the compounds, the particles are intermingled to form an essentially homogeneous powder mixture of the precursors. Such intermingling is preferably conducted by forming a wet mixture using a volatile solvent and then the intermingled particles are pressed together in pellet form in grain-to-grain contact with one another. Although it is desired that the precursor compounds be present in a proportion which provides the stated general formula of the product,

the lithium compound may be present in an excess amount on the order of 5 percent excess lithium compared to a stoichiometric mixture of the precursors. Although a number of lithium compounds are available as precursors, such as lithium acetate, lithium hydroxide, and lithium nitrate, lithium carbonate (Li_2CO_3) is preferred for the solid state reaction. The aforesaid precursor compounds are generally crystals, granules, and powders and are generally referred to as being in particle form. Although many types of phosphate salts are known, it is preferred to use ammonium phosphate $(\text{NH}_4)_2\text{HPO}_4$. In the case where the compound of the formulation $\text{Li}_3\text{M}'\text{M}''(\text{PO}_4)_3$ is desired where M and M' are the same metal, a transition metal, such as vanadium, a suitable precursor is vanadium pentoxide (V_2O_5).

The starting materials are available from a number of sources. The following are typical. Vanadium pentoxide of the general formula V_2O_5 is obtainable from any number of suppliers including Kerr McGee, Johnson Matthey, or Alpha Products of Davers, Massachusetts. It had a melting point of about 690°C , decomposed at 1750°C , a particle size of less than about 60 mesh (250 microns) and had a specific gravity of 3.357 grams per cc at 18°C . It was a yellow-red crystalline powder. Vanadium pentoxide has a CAS number of 1314-62-1. Alternatively, the vanadium pentoxide may be prepared from ammonium metavanadate (NH_4VO_3) . The ammonium metavanadate is heated to a temperature of about 400°C to about 450°C to decompose it to vanadium pentoxide (V_2O_5). Processes for production of vanadium pentoxide are described in U.S. Patent Numbers 3,728,442, 4,061,711 and 4,119,707, each of which is incorporated herein by reference in its entirety.

In another embodiment, for the formation of $\text{Li}_3\text{M}'\text{M}''(\text{PO}_4)_3$, where M' and M'' are different from one another and are metals, preferably transition metals, one may select two different metal oxide powders, such as titanium oxide (TiO_2), vanadium oxide (V_2O_5 , V_2O_3), iron

oxide (FeO , Fe_2O_3), chromium oxide (CrO_2 , CrO , Cr_2O_3), manganese oxide (MnO_2 , Mn_3O_4), cobalt oxide (CoO), nickel oxide (NiO), copper oxide (CuO), molybdenum oxide (MoO_2 , MoO_3) and zinc and zirconium compounds, and the like. In

5 still another embodiment where the formulation $\text{Li}_3\text{M}'\text{M}''(\text{PO}_4)_3$, comprises two different metals, M' and M'' , one metal M' may be selected from non-transition metals and semi-metals. In another embodiment, non-transition metal has only one oxidation state and is nonoxidizable from its oxidation

10 state in the final compound $\text{Li}_3\text{M}'\text{M}''(\text{PO}_4)_3$. In this case, M' may be selected from metals, such as aluminum and magnesium, calcium, potassium, and other Groups I and II metals, alkali Group I, and semi-metals. Semi-metals are located in the Periodic Table on the right hand side and

15 roughly separate the nonmetals from metals, as is well known in the art. In this case, M'' is a metal having more than one oxidation state, and is oxidizable from its oxidation state in the end product, and M'' is preferably a transition metal. Examples are $\text{Li}_3\text{KCr}(\text{PO}_4)_3$ and $\text{Li}_3\text{KMo}(\text{PO}_4)_3$,

20 where the transition metal (Tm) is, respectively, chromium and molybdenum. See also Tables A to G showing exemplary mixed metal combinations, oxidation states on removal of Li, and active material capacity.

25 Example I

A preferred procedure for forming the $\text{Li}_3\text{M}'\text{M}''(\text{PO}_4)_3$ compound active material will now be described. The method for making $\text{Li}_3\text{M}'\text{M}''(\text{PO}_4)_3$ will be illustrated by formation of $\text{Li}_3\text{V}_2(\text{PO}_4)_3$, ($\text{Li}_3\text{M}_2(\text{PO}_4)_3$). The

30 basic procedure comprised conducting a reaction between a lithium compound, preferably lithium carbonate (Li_2CO_3), a metal oxide, preferably vanadium pentoxide (V_2O_5), and a phosphoric acid derivative, preferably the phosphoric acid ammonium acid salt, ammonium phosphate, $\text{NH}_4\text{H}_2(\text{PO}_4)$ or

35 $(\text{NH}_4)_2\text{H}(\text{PO}_4)$. Each of the precursor starting materials are available from a number of chemical outfits including

Aldrich Chemical Company and Fluka. The $\text{Li}_3\text{V}_2(\text{PO}_4)_3$ was prepared with approximately a stoichiometric mixture of Li_2CO_3 , V_2O_5 , and $(\text{NH}_4)_2\text{HPO}_4$. However, a 5 percent excess of lithium (as lithium carbonate) was used to minimize any lithium loss as (Li_2O) . The precursor materials were initially intimately mixed and ground for about 30 minutes in a methanol solution. The intimately mixed compounds were then dried and pressed into pellets. Reaction was conducted by heating in an oven at a preferred ramped heating rate of 1°C per minute up to a temperature of about 725°C , and held at 725°C for about 12 hours to decompose the carbonate. Then heating continued at the same ramp rate (1°C per minute) up to a temperature of about 875°C . The mixture was held at this temperature for about 24 hours. The entire reaction was conducted in a reducing atmosphere under flowing pure hydrogen gas. The flow rate will depend upon the size of the oven and the quantity needed to maintain a reducing atmosphere. Based on the size of the oven used in this example a flow rate of 25 cubic centimeters per minute was used. The oven was permitted to cool down at the end of the 24 hour period, where cooling occurred at a rate of about 3°C per minute. Then the entire procedure was repeated once again for a further 24 hours. The repeated steps were also conducted under reducing atmosphere. Although hydrogen gas was selected to provide the reducing atmosphere, other means for obtaining the reducing atmosphere may be used.

The general aspects of the above synthesis route are applicable to a variety of starting materials. For example, LiOH and LiNO_3 salts may replace Li_2CO_3 as the source of lithium. In this case, the temperature for the first step will vary due to the differing melting points, 450°C for LiOH and 700°C for LiNO_3 . The vanadium oxide V_2O_5 (V^{+5}), combined with the oxidizing power of the phosphate anion, is required to be offset by a strong reducing agent, for example, the hydrogen atmosphere. Alternatively, lower

oxidation state vanadium complexes could be used, e.g., V_2O_3 . This is a vanadium in the 3+ state. But because of the presence of PO_4 , a certain degree of oxidation might occur. Therefore, a reducing agent is used. For example, a mixture of 90:10 of $Ar:H_2$ can be used. The same considerations apply to other lithium-metal- and phosphate-containing precursors. The relative oxidizing strength of the selected precursors, and the melting point of the salts will cause adjustment in the general procedure, such as, selection of the reducing agent, its reducing capability and flow rate, and the temperature of reaction.

The final product appeared lime-green in color, and its $CuK\alpha$ x-ray diffraction pattern contained all of the peaks expected for this material as shown in Figure 6. The x-ray diffraction was conducted using $CuK\alpha$ radiation, $\lambda = 1.5418 \text{ \AA}$. The pattern evident in Figure 6 is consistent with a single oxide compound $Li_3V_2(PO_4)_3$. This is evidenced by the position of the peaks in terms of the scattering angle 2θ (theta), x axis. The x-ray pattern showed no peaks due to the presence of precursor oxides indicating that the solid state reaction is essentially entirely completed. Chemical analysis for lithium and vanadium by atomic absorption spectroscopy showed, on a percent by weight basis, 5.17 percent lithium and 26 percent vanadium. This is close to the expected result of 5.11 percent lithium and 25 percent vanadium.

The chemical analysis and x-ray pattern demonstrate that the product of the invention was indeed the nominal general formula $Li_3V_2(PO_4)_3$, corresponding to the more generic nominal general formula $Li_3M'M''(PO_4)_3$. The term "nominal general formula" refers to the fact that the relative proportion of atomic species may vary slightly on the order of 2 percent to 5 percent, or more typically, 1 percent to 3 percent.

35

Example II

The $\text{Li}_3\text{V}_2(\text{PO}_4)_3$, prepared as described immediately above, was tested in an electrochemical cell. The positive electrode was prepared as described above under the section designated "Positive Electrode". The negative electrode was metallic lithium. The electrolyte was a 2:1 weight ratio mixture of ethylene carbonate and dimethyl carbonate within which was dissolved 1 molar LiPF_6 . The cell was cycled between about 3.0 and about 4.3 volts with performance as shown in Figures 1, 2, 3, 4A, and 4B.

Figure 1 shows a voltage profile of the test cell, based on the $\text{Li}_3\text{M}'\text{M}''(\text{PO}_4)_3$ positive electrode active material of the invention, and using a lithium metal counter electrode as described in the examples. The data shown in Figure 1 is based on the Electrochemical Voltage Spectroscopy (EVS) technique. Electrochemical and kinetic data were recorded using the Electrochemical Voltage Spectroscopy (EVS) technique. Such technique is known in the art as described by J. Barker in Synth, Met 28, D217 (1989); Synth. Met. 32, 43 (1989); J. Power Sources, 52, 185 (1994); and Electrochemical Acta, Vol. 40, No. 11, at 1603 (1995). Figure 1 clearly shows and highlights the very high and unexpected degree of reversibility of the lithium ion reactions of the $\text{Li}_3\text{M}'\text{M}''(\text{PO}_4)_3$, specifically $\text{Li}_3\text{V}_2(\text{PO}_4)_3$, active material of the invention. The positive electrode contained about 16.8 milligrams of the $\text{Li}_3\text{V}_2(\text{PO}_4)_3$ active material. The total electrode weight including the binder and conductive carbon diluent was about 31.2 milligrams. The positive electrode showed a performance of about 136 milliamp hours per gram on the first discharge. In Figure 1, the capacity in is essentially 136 milliamp hours per gram, and the capacity out is essentially 131 milliamp hours per gram, resulting in essentially no capacity change. Figure 2 is an EVS differential capacity plot based on Figure 1. As can be seen from Figure 2, the relatively symmetrical nature of peaks indicates good

electrical reversibility, with none related to irreversible reactions, since all peaks above the axis (cell charge) have corresponding peaks below the axis (cell discharge), and there is essentially no separation between the peaks
5 above and below the axis.

Figure 3 shows the results of the first constant current cycling at 0.20 milliamps per square centimeter between about 3.0 and 4.3 volts based upon about 16.8 milligrams of the $\text{Li}_3\text{V}_2(\text{PO}_4)_3$ active material in the cathode
10 (positive electrode). In an as prepared, as assembled, initial condition, the positive electrode active material is $\text{Li}_3\text{V}_2(\text{PO}_4)_3$. The lithium is deintercalated from the $\text{Li}_3\text{V}_2(\text{PO}_4)_3$ during charging of the cell. When fully charged, about 2 units of lithium have been removed per
15 formula unit of the original lithium-vanadium-phosphate. Consequently, the positive electrode active material corresponds to $\text{Li}_{3-x}\text{V}_2(\text{PO}_4)_3$, where x is greater than 0 and less than 3, and in the operation of this cell, x appears to be equal to about 2, when the cathode material is at 4.2
20 volts versus Li/Li^+ . In this charged condition, the electrochemical potential versus lithium of the $\text{Li}_3\text{V}_2(\text{PO}_4)_3$ is about 4.2 volts. The deintercalation of 2 lithium from $\text{Li}_3\text{V}_2(\text{PO}_4)_3$ resulting in the $\text{Li}_1\text{V}_2(\text{PO}_4)_3$, represents approximately 127 milliamp hours per gram corresponding to
25 about 2.2 milliamp hours based on 16.8 milligrams active material. Next, the cell is discharged whereupon a quantity of lithium is reintercalated into the $\text{Li}_1\text{V}_2(\text{PO}_4)_3$. The average voltage is approximately 3.8 volts versus Li/Li^+ . The reintercalation corresponds to approximately
30 101 milliamp hours per gram proportional to the intercalation of about 1.54 atomic units of lithium. The bottom of the curve corresponds to approximately 3.0 volts.

Figure 4 presents data obtained by multiple constant current cycling at 0.25 milliamp hours per square
35 centimeter of the $\text{Li}_3\text{V}_2(\text{PO}_4)_3$ versus lithium metal counter electrode between 3.0 and 4.2 volts using the electrolyte

and with electrodes formed as described earlier and with an initial specific capacity of 115 milliamp hours per gram. Figure 4 is a two part graph with Figure 4A showing the excellent rechargeability of the $\text{Li/Li}_3\text{V}_2(\text{PO}_4)_3$ cell. Figure 4B shows good cycling and capacity of the cell. The performance shown after 113 cycles is good and shows that electrode formulations of the type $\text{Li}_3\text{M}'\text{M}''(\text{PO}_4)_3$ are very desirable.

It should be noted that the formulations obtained by the method of the invention demonstrated capacity less than the achievable theoretical capacity. This is because the method of preparation and cell configurations have not yet been optimized for this remarkable material. Nevertheless, this material is highly desirable as an active material to replace the widely used LiMn_2O_4 , Li_2CoO_2 , and LiNiO_2 , as can be seen by considering its theoretical capacity. The theoretical specific capacity for $\text{Li}_3\text{V}_2(\text{PO}_4)_3$ is about 190 milliamp hours per gram. This is based on extracting all 3 lithium from the original starting material. Actually, the theoretical capacity is closer to about 197 milliamp hours per gram corresponding to about 66 milliamp hours for each atomic unit of lithium extracted from the $\text{Li}_3\text{V}_2(\text{PO}_4)_3$ compound. Assuming that each such extracted unit of lithium corresponds to 66 milliamp hours, it can be seen that in Figure 1 the charge extracted of 136 milliamp hours per gram corresponds to the extraction of slightly more than 2 units of lithium from the $\text{Li}_3\text{V}_2(\text{PO}_4)_3$.

Example III (Hexagonal $\text{Li}_3\text{AlV}(\text{PO}_4)_3$)

A method for making $\text{Li}_3\text{AlV}(\text{PO}_4)_3$ will now be described. The basic procedure comprises conducting a reaction between lithium carbonate, aluminum hydroxide, vanadium oxide, and ammonium phosphate according to the reaction below.

35





The precursor materials were initially intimately mixed and ground as described with respect to Example 1. After mixing, the mixed precursor powders were compressed into tablet form and then heated at about 250°C for about 6 hours under an argon atmosphere. Then the temperature was raised to 600°C where heating was conducted for 12 hours, also under argon. Next, the pellets were cooled, ground and repelletized. Next, heating was conducted for about 15 hours at a temperature of about 940°C under argon atmosphere.

The final product was subjected to CuK alpha X-ray diffraction as described with respect to Example 1. The unit cell parameters are as described in Table H.

The chemical analysis and X-ray pattern demonstrated that the product of the invention was indeed the nominal general formula $\text{Li}_3\text{AlV}(\text{PO}_4)_3$.

20 Example IV

The $\text{Li}_3\text{AlV}(\text{PO}_4)_3$, prepared as described immediately above, was tested in an electrochemical cell, the positive electrode was prepared as described under the section designated "positive electrode." The negative electrode was metallic lithium. The cell was prepared and cycled as generally described with respect to Example II above.

Figure 7 shows a voltage profile of the test cell based on the electrochemical voltage spectroscopy (EVS) technique, as described with respect to Example II above. Figure 7 clearly shows and highlights the very high and unexpected degree of reversibility of lithium ion reactions of this compound. As in the case of Examples I and II, the material as prepared, is capable of first deintercalating lithium and then reintercalating lithium for functioning reversibly in an ion cell. Figure 8 is an EVS differential capacity plot based on Figure 7. As can be seen from

Figure 8, the relatively symmetrical nature of the peaks indicates good electrochemical reversibility.

Figure 9 shows the results of the first constant current cycling at plus/minus 0.05 milliamps per square centimeter between about 3 and 4.5 volts based on the $\text{Li}_{3-x}\text{AlV}(\text{PO}_4)_3$ active material in the cathode (positive electrode). In an as-prepared, as-assembled initial condition, the positive electrode active material contains 3 lithium, most being capable of deintercalation. The lithium is deintercalated from the material during charging of the cell. This material demonstrated about 35 milliamp hours per gram when removing about 0.5 lithium per formula unit per cycle. It was possible to reintercalate all of the lithium which had been previously taken out in the first half cycle.

Figure 10 shows data obtained by multiple constant current cycling at plus/minus 0.05 milliamps per square centimeter versus metallic lithium counter-electrode. This graph shows good reversible cycling over eight cycles. This demonstrates good cycling and capacity of the cell.

Example V

The electrode material prepared in accordance with Example 1 was tested in an electrochemical cell against a negative electrode which was a carbon active material designated MCMB2528. MCMB2528 is a mesocarbon microbead material supplied by Alumina Trading, which is the U.S. distributor for the supplier, Osaka Gas Company of Japan. This material has a density of about 2.24 grams per cubic centimeter; a particle size maximum for at least 95% by weight of the particles of 37 microns; median size of about 22.5 microns and an interlayer distance of about 0.336. Figure 11 shows results similar to that described with respect to Examples I and II. In an as-prepared, as-assembled initial condition, the positive electrode active

material is $\text{Li}_3\text{V}_2(\text{PO}_4)_3$. The lithium is deintercalated from this active material during charging of the cell. During charging, lithium is removed from the lithium vanadium phosphate and intercalated into the MCMB carbon material.

5 Here, the positive electrode and negative electrode active materials were not optimized. There was not a sufficient quantity of the lithium vanadium phosphate to balance the amount of carbon material in the negative electrode. Yet, the cathode utilization was surprisingly good. Figure 11

10 shows that about 120 milliamp hours per gram was extracted from the positive electrode material of the invention and about 95 milliamp hours per gram was observed on first discharge. This indicates that essentially all of the lithium extracted from the lithium vanadium phosphate was

15 able to be reinserted in the second part of the cycle.

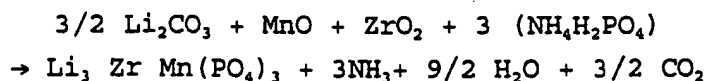
Figure 12 presents data obtained by multiple constant current cycling at about plus/minus 0.2 milliamps per square centimeter of the lithium vanadium phosphate of Example 1 versus the MCMB carbon negative electrode, between about 2.5 and 4.1 volts. Figure 12 shows excellent rechargability of the carbon/ $\text{Li}_3\text{V}_2(\text{PO}_4)_3$ cell; with performance through 10 cycles being very good.

20

Example VI

25 A material of the general formula $\text{Li}_3\text{MnZr}(\text{PO}_4)_3$ was prepared from the precursors lithium carbonate, manganese oxide, zirconium oxide, and the ammonium dihydrogen phosphate. This reaction was conducted in accordance with the reaction shown below.

30



The procedure was followed similar to that described with respect to Example III. The precursor

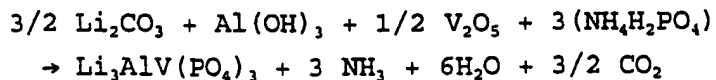
35 powders were mixed and then pelletized. They were then

heated for about 6 hours at temperature of about 250°C under argon. Next, the temperature was elevated to 600°C and heating was conducted for about 12 hours under argon. The pellets were permitted to cool and then they were
5 ground and repelletized. Then heating was conducted for another 15 hours at a temperature of about 940°C under argon.

This procedure is similar to that described for the analogous sodium compounds $\text{Na}_3\text{MnZr}(\text{PO}_4)_3$, $\text{Na}_3\text{MgZr}(\text{PO}_4)_3$,
10 as reported by Feltz and Barth in Solid State Ionics 9-10 (1983) pp. 817-822. These compounds may be prepared by the method described by Feltz and Barth in the sodium form and the lithium form is prepared by ion substitution by well known methods. Direct preparation using lithium precursors
15 as described above, and consistent with the methods of Feltz and Barth, is preferred. However, it should be noted that the preparation methods of Feltz and Barth are conducted in an air atmosphere. The effects of the atmosphere on the product characteristics are described
20 below. Such relationship is based on the data given above in the examples related to hydrogen and argon atmosphere. Another example using hydrogen atmosphere follows immediately below.

25 Example VII (Orthorhombic $\text{Li}_3\text{AlV}(\text{PO}_4)_3$)

The procedure for forming the orthorhombic $\text{Li}_3\text{AlV}(\text{PO}_4)_3$ was generally as per Example III, except that a different atmosphere was used for the heating steps and the vanadium oxide precursor differed. The reaction was as
30 given below.



35 Here, V_2O_5 was used in place of the V_2O_3 of Example III. All heating steps in this Example VII were

carried out under H_2 (hydrogen) gas atmosphere. Essentially 100% H_2 atmosphere was achieved using flowing H_2 gas. The product of this Example VII (orthorhombic) had different structure and electrochemical performance as compared to Example III (hexagonal). See Table I for unit cell parameters obtained by CuK-alpha x-ray diffraction.

Example VIII

The $Li_3AlV(PO_4)_3$, prepared as per Example VII above, was tested in an electrochemical cell, the positive electrode was prepared as described under the section designated "positive electrode." The negative electrode was metallic lithium. The cell was prepared and cycled as generally described with respect to Example II above.

Figure 13 shows a voltage profile of the test cell based on the electrochemical voltage spectroscopy (EVS) technique, as described with respect to Example II above. Figure 13 clearly shows a very high degree of reversibility of lithium ion reactions of this orthorhombic structure. The material as prepared, is capable of first deintercalating lithium and then reintercalating lithium for functioning reversibly in an ion cell. Figure 14 is an EVS differential capacity plot based on Figure 13. Figure 14 shows a profile different from the hexagonal form of this compound as per Figure 8.

Figure 15 shows the results of the first constant current cycling at plus/minus 0.05 milliamps per square centimeter between about 3 and 4.2 volts based on the $Li_3AlV(PO_4)_3$ active material in the cathode (positive electrode). This material demonstrated about 55 milliamp hours per gram, and permitted removing more lithium per cycle than the product of Example III.

A comparison of Figures 9 and 15 reveals that the orthorhombic $Li_3AlV(PO_4)_3$ (Fig. 15) had better performance, higher specific capacity, i.e., better cathode utilization

than the hexagonal $\text{Li}_3\text{AlV}(\text{PO}_4)_3$ of Fig. 9. Recall that the $\text{Li}_3\text{AlV}(\text{PO}_4)_3$ of Fig. 9 was prepared under argon using V_2O_5 and the $\text{Li}_3\text{AlV}(\text{PO}_4)_3$ of Fig. 15 was prepared under H_2 gas using V_2O_5 . In the latter process, V_2O_5 is thought to be
5 reduced in situ to V_2O_3 under hydrogen.

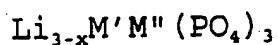
The benefits of the H_2 gas atmosphere, a reducing atmosphere, were also observed in the preparation of the $\text{Li}_3\text{V}_2(\text{PO}_4)_3$ when compared to the same product prepared under argon. The argon-prepared $\text{Li}_3\text{V}_2(\text{PO}_4)_3$ originated from a V_2O_5 precursor and had first charge-discharge cycle specific
10 capacity of 105 mAh/g out (lithium extracted) and 80 mAh/g in (lithium inserted). The H_2 -prepared $\text{Li}_3\text{V}_2(\text{PO}_4)_3$ originated from a V_2O_5 precursor and had first charge-discharge cycle specific capacity of 136 mAh/g out (lithium
15 extracted) and 131 mAh/g in (lithium inserted) as per Examples I and II.

There is no known prior attempt to deintercalate lithium from a lithium-containing metal phosphate. Thus, the electrochemical reaction demonstrated by the present
20 invention is remarkable as it has not heretofore been suggested. The product of the present invention may be compared to a Nasicon ($\text{Na}_3\text{Zr}_2\text{PSi}_2\text{O}_{12}$) framework which is a skeleton structure with an interconnected interstitial space. There are also the Langbeinite-type ($\text{K}_2\text{Mg}_2(\text{SO}_4)_3$)
25 structures which are true cage structures. Such structures do not permit mobility of mobile metal ions through the crystal. Some Nasicon-type structures possess ionic conductivity but have very poor electronic conductivity. Some Nasicon-type structures are usable as solid
30 electrolytes, but are not usable as electrode materials. This is because they lack an oxidizable metal in their structure, therefore, an ion cannot be extracted. Thus, such structures and compounds are useless for ion battery, rocking chair battery, application.

35 In contrast to the known art, the present invention provides a lithium-metal-phosphate compound

having an oxidizable metal. Such metal is capable of more than one oxidation state. The metal is present in the lithium-metal-phosphate compound at less than its highest oxidation state. Therefore, the metal is oxidizable to provide capability to extract out one or more Li^+ ions. This is demonstrated by oxidation of V in $\text{Li}_3\text{V}_2(\text{PO}_4)_3$ from $\text{V}^{3+}\text{V}^{3+}$ to $\text{V}^{4+}\text{V}^{5+}$. It should be noted that based on formation as described herein, there are many combinations. See Tables A to I. The oxidation states for many compounds of the invention are as per the examples and tables. Note that the amount of Li^+ removed or added will determine the relative oxidation state of E' and E'' or M' and M'' . For example, Fe in $\text{Li}_3\text{Fe}_2(\text{PO}_4)_3$ from $\text{Fe}^{3+}\text{Fe}^{3+}$ to $\text{Fe}^{4+}\text{Fe}^{4+}$; Mn in $\text{Li}_3\text{Mn}_2(\text{PO}_4)_3$ from $\text{Mn}^{3+}\text{Mn}^{3+}$ to $\text{Mn}^{4+}\text{Mn}^{4+}$; and other $\text{Li}_3\text{M}_1\text{M}_2(\text{PO}_4)_3$, as per $\text{Fe}^{3+}\text{Ti}^{3+}$ to $\text{Fe}^{4+}\text{Ti}^{4+}$; $\text{Co}^{3+}\text{Mn}^{3+}$ to $\text{Co}^{4+}\text{Mn}^{4+}$; $\text{Cu}^{2+}\text{Mn}^{4+}$ to $\text{Cu}^{3+}\text{Mn}^{4+}$, and $\text{Fe}^{3+}\text{V}^{3+}$ to $\text{Fe}^{4+}\text{V}^{4+}$.

Table A.



M' = Non transition metal initial oxidation state = +3

M'' = Transition metal initial oxidation state = +3

5	<u>M'M''</u>	<u>RMM</u>	<u>No. of Li's</u> <u>Removed</u>	<u>mAh/g</u>
	Al Ti	381	1	70
	Al V	384	2	140
	Al Cr	385	3	209
	Al Mn	388	1	69
10	Al Fe	389	1	69
	Al Co	392	1	68
	Al Ni	392	1	68
	Al Cu	397	1	68
15	B Ti	365	1	73
	B V	368	2	146
	B Cr	369	3	218
	B Mn	372	1	72
	B Fe	373	1	72
20	B Co	376	1	71
	B Ni	376	1	71
	B Cu	381	1	70

25 Note: Refer to footnotes 3 and 4 of Table C

Table B. $\text{Li}_{3-x} \text{M}'\text{M}'' (\text{PO}_4)_3$

M' = Non transition metal initial oxidation state = +2

M'' = Transition metal initial oxidation state = +4

5	<u>M'M"</u>	<u>RMM</u>	<u>No. of Li's</u> <u>Removed</u>	<u>mAh/g</u>
	Mg V	381	1	70
	Mg Mo	426	2	126
	Mg Cr	382	2	140
10	Ca V	397	1	68
	Ca Mo	442	2	121
	Ca Cr	398	2	135

15 Note: Refer to footnotes 3 and 4 of Table C

Table C. $\text{Li}_{3-x} \text{M}^{\text{II}} \text{M}^{\text{IV}} (\text{PO}_4)_3$ $\text{M}^{\text{IV}} = \text{Zr, Ti}$ $\text{M}^{\text{II}} = \text{Any transition metal capable of +2 oxidation state}$

5

	<u>M^{II} (1)</u>	<u>$\text{M}^{\text{II}} \text{M}^{\text{IV}}$ (2)</u>	<u>RMM</u>	<u>No. of Li's</u>	<u>mAh/g</u>
	<u>Ionic radius</u>			<u>Removed</u>	
	67 pm	Mn Zr	452	2	119
	86 pm	Ti Zr	445	2	120
10	79 pm	V Zr	448	3	180
	80 pm	Cr Zr	449	3	179
	78 pm	Fe Zr	453	2	118
	74 pm	Co Zr	456	2	118
	69 pm	Ni Zr	456	2	118
15	73 pm	Cu Zr	461	1	58
	69 pm	Mo Zr	493	3	163
	67 pm	Mn Ti	409	2	131
	86 pm	Ti Ti	402	2	133
	79 pm	V Ti	405	3	199
20	80 pm	Cr Ti	406	3	199
	78 pm	Fe Ti	410	2	131
	74 pm	Co Ti	413	2	130
	69 pm	Ni Ti	413	2	130
	73 pm	Cu Ti	418	1	64
25	69 pm	Mo Ti	450	3	178

(1) Taken from R.D. Shannon, Acta Cryst. A32, 751 (1976).

- (2) In each case the M^{II} oxidizes to higher oxidation state in proportion to the amount of Li removed, because the Zr^{IV} and the Ti^{IV} do not oxidize.
- 5 (3) RMM is relative molecular mass.
- (4) The term "No. of Li's Removed" is on a per formula unit basis.
- 10

Table D. $\text{Li}_{3-x}\text{Sn}^{\text{I}}\text{M}^{\text{IV}}(\text{PO}_4)_3$ M^{IV} = Transition metal oxidation state = +4

5	<u>Sn M^{IV}</u>	<u>RMM</u>	<u>No. of Li's</u> <u>Removed</u>	<u>Oxidations</u>	<u>mAh/g</u>
	Sn V	476	3	$\text{Sn}^{2+} \rightarrow \text{Sn}^{4+}$ $\text{V}^{4+} \rightarrow \text{V}^{5+}$	169
	Sn Cr	477	3	$\text{Sn}^{2+} \rightarrow \text{Sn}^{4+}$ $\text{Cr}^{4+} \rightarrow \text{Cr}^{5+}$	169
	Sn Mo	521	3	$\text{Sn}^{2+} \rightarrow \text{Sn}^{4+}$ $\text{Mo}^{4+} \rightarrow \text{Mo}^{5+}$	154

Note: Refer to footnotes 3 and 4 of Table C.

10 The designation of oxidation pertains to expected performance based on analogy to corresponding results achieved as per the Examples.

Table E. $\text{Li}_{3-x} \text{Pb}^{\text{II}} \text{M}^{\text{IV}} (\text{PO}_4)_3$

	<u>RMM</u>	<u>Li's Removed</u>	<u>Oxidations</u>	mAh/g
PbV	564	3	$\text{Pb}^{2+} \rightarrow \text{Pb}^{4+}$ $\text{V}^{4+} \rightarrow \text{V}^{5+}$	143
PbCr	565	3	$\text{Cr}^{4+} \rightarrow \text{Cr}^{5+}$ $\text{Pb}^{2+} \rightarrow \text{Pb}^{4+}$	142
5 PbMo	609	3	$\text{Pb}^{2+} \rightarrow \text{Pb}^{4+}$ $\text{Mo}^{4+} \rightarrow \text{Mo}^{5+}$	132

Note: Refer to all footnotes of Table D.

Table F. $\text{Li}_{3-x}\text{SnM}^{\text{IV}}(\text{PO}_4)_3$ $\text{M}^{\text{IV}} = \text{Zr, Ti}$

		<u>RMM</u>	<u>Li's Removed</u>	<u>Oxidation</u>	<u>mAh/g</u>
5	SnZr	516	2	$\text{Sn}^{2+} \rightarrow \text{Sn}^{4+}$	104
	SnTi	473	2	$\text{Sn}^{2+} \rightarrow \text{Sn}^{4+}$	113

10

Table G. $\text{Li}_{3-x}\text{PbM}^{\text{IV}}(\text{PO}_4)_3$

		<u>RMM</u>	<u>Li's Removed</u>	<u>Oxidation</u>	<u>mAh/g</u>
15	PbZr	604	2	$\text{Pb}^{2+} \rightarrow \text{Pb}^{4+}$	89
	PbTi	561	2	$\text{Pb}^{2+} \rightarrow \text{Pb}^{4+}$	96

20

Note: Refer to all footnotes of Table D.

Table H. $\text{Li}_3\text{AlV}(\text{PO}_4)_3$ $\text{Li}_3\text{AlV}(\text{PO}_4)_3$ Fit to a Hexagonal Unit Cell

A = 9.383871 .034458 A Alpha = 90.000000 Degrees

5 B = 9.383871 .034458 A Beta = 90.000000 Degrees

C = 24.841420 .118174 A Gamma = 120.000000 Degrees

Unit cell volume = 1894.40 cubic angstroms

	H	K	L	SST-OBS	SST-CALC
	1	0	2	.012937	.012831
10	1	1	0	.026589	.026953
	1	1	2	.031495	.030800
	0	0	6	.034983	.034615
	2	0	2	.040351	.039784
	0	0	7	.047178	.047115
15	2	0	4	.051993	.051323
	1	0	7	.055883	.056100
	2	1	0	.063080	.062891
	2	1	2	.065955	.066738
	1	0	9	.085993	.086869
20					

Table I. $\text{Li}_3\text{AlV}(\text{PO}_4)_3$,
 $\text{Li}_3\text{AlV}(\text{PO}_4)_3$, Fit to an Orthorhombic Unit Cell

5	A = 7.947642 .004678 A Alpha = 90.000000 Degrees B = 21.493340 .012984 A Beta = 90.000000 Degrees C = 6.983464 .004729 A Gamma = 90.000000 Degrees Unit cell volume = 1185.24 cubic angstroms				
	H	K	L	SST-OBS	SST-CALC
10	1	3	0	.020869	.020954
	1	3	1	.033500	.033279
	2	0	0	.037402	.037575
				.040448	
	1	5	0	.041766	.041505
15	0	6	0	.046122	.046240
	0	2	2	.054563	.054438
	2	4	0	.058276	.058126
	0	6	1		.058565
				.066397	
20	1	6	1	.067686	.067958
	2	4	1	.070720	.070451
	1	4	2	.079475	.079245
	2	6	0	.083848	.083815
	2	0	2	.086672	.086876
25	0	6	2	.095410	.095540
	2	7	0	.100296	.100512
	0	1	3		.112211
	0	7	2	.112303	.112238
	1	9	0	.113604	.113433
30				.124763	
	3	3	2	.145561	.145405
	0	6	3	.156832	.157166
	3	5	2		.165956
	2	10	0	.166092	.166018
35	1	6	3		.166560
	0	8	3	.193220	.193130
	1	3	4	.218344	.218156

Lithium ion batteries made with this technology are made in the discharged state, also referred to as pre-charge (before charge) state. They require a conditioning charge before use. In the initial condition (pre-charge state), anodes of lithium ion batteries are essentially free of lithium, and often free of ions thereof, as in the case of graphite. Therefore, such batteries, in the initial condition (as-assembled) pre-charge state, are inherently more stable and relatively less reactive than batteries containing lithium metal, or containing fully or partially charged anodes. The active materials themselves are also inherently air stable.

To achieve a useable potential difference, the (positive electrode) is electrochemically oxidized, while the anode (negative electrode) is reduced. Thus, during charging, a quantity (x) of lithium ions (Li^+) leave the positive electrode, $\text{Li}_{3-x}\text{M}'_y\text{M}''_{2-y}(\text{PO}_4)_3$, and the positive electrode is oxidized, increasing its potential; during charging, the Li ions are accepted at or intercalated into a negative electrode, preferably a carbon-based negative electrode, which is reduced. As a result, the negative electrode has a potential very close to the lithium metal potential, which is zero volts. A typical graphite electrode can intercalate up to about 1 atom of lithium per each of 6 carbons, that is, Li_0C_6 to Li_1C_6 . During discharging, the reverse occurs, and a quantity of (x) of lithium (Li^+) ions leave the negative electrode, increasing its potential. During discharge, the lithium ions are accepted (intercalated) back into the positive electrode, which is reduced, and its potential is reduced. If the $\text{Li}_3\text{M}'_y\text{M}''_{2-y}(\text{PO}_4)_3$ compound were used as a negative electrode, during charge, Li ions would be transferred to the negative electrode, as $\text{Li}_{3+x}\text{M}'_y\text{M}''_{2-y}(\text{PO}_4)_3$, and the M' , M'' , or both, would theoretically achieve a higher oxidation state. On discharge, the Li^+ ions would be transferred back to the positive electrode.

The compounds of the invention are also characterized by being air stable in an as-prepared condition. This is a striking advantage, because it facilitates preparation of and assembly of battery cathodes and cells, without the requirement for controlled atmosphere. This feature is particularly important, as those skilled in the art will recognize that air stability, that is, lack of degradation on exposure to air, is very important for commercial processing. Air-stability is known in the art to more specifically indicate that a material does not hydrolyze in presence of moist air. Generally, air-stable materials are also characterized by extracting Li above about 3.0 volts versus lithium. The higher the extraction potential, the more tightly bound the lithium ions are to the host lattice. This tightly bound property generally confers air stability on the material. The air-stability of the $\text{Li}_x\text{M}'\text{M}''(\text{PO}_4)_3$ materials of the invention is consistent with the stability demonstrated for $\text{Li}_x\text{V}_2(\text{PO}_4)_3$ by constant current cycling at 0.20 milliamps per square centimeter between about 3 and 4.2 volts versus Li metal anode. If a material intercalates Li below about 3.0 volts versus lithium, it is generally not air-stable, and it hydrolyzes in moist air.

While this invention has been described in terms of certain embodiments thereof, it is not intended that it be limited to the above description, but rather only to the extent set forth in the following claims.

The embodiments of the invention in which an exclusive property or privilege is claimed are defined in the following claims.

Valence 2078/79

Claims:

1. A lithium ion battery comprising: a first electrode having an active material in a first condition of the nominal general formula $\text{Li}_{3-x}\text{M}'_y\text{M}''_{2-y}(\text{PO}_4)_3$, $x = 0$, $0 \leq y \leq 2$, and in a second condition of the nominal general formula $\text{Li}_{3-x}\text{M}'_y\text{M}''_{2-y}(\text{PO}_4)_3$, $0 < x \leq 3$; M'' is a transition metal, and M' is a non-transition-metal element selected from the group consisting of metals and metalloids; a second electrode which is a counter-electrode to said first electrode; and an electrolyte between said electrodes.

2. The battery of claim 1 wherein M' is selected from the group consisting of Mg, Be, Ca, Sn, Pb, Ge, B, K, Al, Ga, In, As, and Sb.

3. The battery of claim 1 wherein M'' is selected from the group consisting of Ti, V, Cr, Mn, Fe, Co, Ni, Cu, Mo, W, Zn, Cd, and Pd.

4. A lithium ion battery comprising: a first electrode having an active material in a first condition of the nominal general formula $\text{Li}_{3-x}\text{M}'_y\text{M}''_{2-y}(\text{PO}_4)_3$, $x = 0$, $0 \leq y \leq 2$, and in a second condition of the nominal general formula $\text{Li}_{3-x}\text{M}'_y\text{M}''_{2-y}(\text{PO}_4)_3$, $0 < x \leq 3$; M' is Zr or Ti; and M'' is a metal characterized by having a +2 oxidation state when $x = 0$; a second electrode which is a counter-electrode to said first electrode; and an electrolyte between said electrodes.

5. The battery of claim 4 wherein said Zr or Ti has a +4 oxidation state in said compound, corresponding to $\text{Li}_{(3-x)}\text{M}'_y\text{M}''_{(2-y)}^{\text{IV}}(\text{PO}_4)_3$.

6. The battery of claim 4 wherein M" is a transition metal.

7. The battery of claim 4 wherein M" is selected from the group consisting of Ti, V, Cr, Mn, Fe, Co, Ni, Cu, Sn, Pb, Mo, W, and Pd.

8. The battery of claim 4 wherein said second electrode active material is selected from the group consisting of carbon, graphite, and mixtures thereof.

9. A lithium ion battery which comprises a positive electrode and a negative electrode; said negative electrode comprising an active material consisting of an intercalation material in a pre-charge state; said positive electrode having an active material comprising a phosphorous compound of the nominal general formula $\text{Li}_x\text{M}'_y\text{M}''_{2-y}(\text{PO}_4)_3$, $y \leq 0 \leq 2$; wherein M' and M'' are the same or different from one another and are each elements selected from the group consisting of metals and metalloids; and wherein said compound deintercalates lithium ions during charging cycle of said battery; said negative electrode active material characterized by intercalating said deintercalated lithium ions during said charging cycle and by subsequent deintercalation of lithium ions during discharge cycle; and said compound characterized by reintercalating said discharge cycle lithium ions.

10. The battery of claim 9 wherein M'' is a transition metal.

11. The battery of claim 9 wherein M'' is a transition metal, and M' is a non-transition-metal metal,

12. The battery of claim 9 wherein M' is selected from the group consisting of Mg, Be, Ca, Sn, Pb, Ge, B, K, Al, Ga, In, As, and Sb.

13. The battery of claim 9 wherein M" is selected from the group consisting of Ti, V, Cr, Mn, Fe, Co, Ni, Cu, Mo, W, Zn, Cd, and Pd.

14. The battery of claim 9 wherein M' is Zr or Ti; and M" is a metal characterized by having a +2 oxidation state.

15. The battery of claim 14 wherein said Zr or Ti has a +4 oxidation state in said compound, corresponding to $\text{Li}_{3-x}\text{M}'^{\text{IV}}\text{M}''_{(2-y)}(\text{PO}_4)_3$; and said M" is a transition metal.

16. The battery of claim 9 wherein said second electrode active material is a carbonaceous material.

17. The battery of claim 9 wherein said second electrode active material is selected from the group consisting of carbon, graphite, and mixtures thereof.

18. The battery of claim 9 wherein, during charging cycle of said battery, the oxidation state of at least one of said M' and M" in said compound increases in relation to said lithium ions (x) deintercalated from said compound during said charging cycle, $0 < x \leq 3$.

19. A method of chemically preparing a product of the nominal formula $\text{Li}_3\text{M}'_y\text{M}''_{2-y}(\text{PO}_4)_3$, $0 \leq y \leq 2$ where M' and M" are each independently selected from the group of metals, comprising the steps of:

- a. intermingling particles of at least one metal oxide compound, particles

of a lithium compound, and particles of a phosphate salt compound, said compounds being in a proportion which provides said nominal formula proportion; and

- b. reacting said compounds in the presence of a non-oxidizing atmosphere to provide said product.

20. The method of claim 19 wherein said phosphate salt compound is ammonium phosphate; said lithium compound is lithium carbonate; said at least one metal oxide compound includes V_2O_5 and; said non-oxidizing atmosphere is a reducing atmosphere.

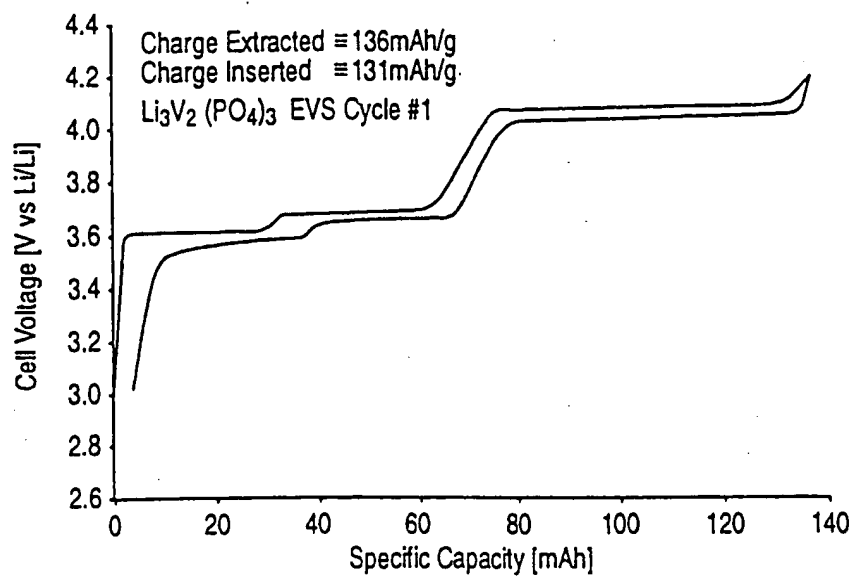
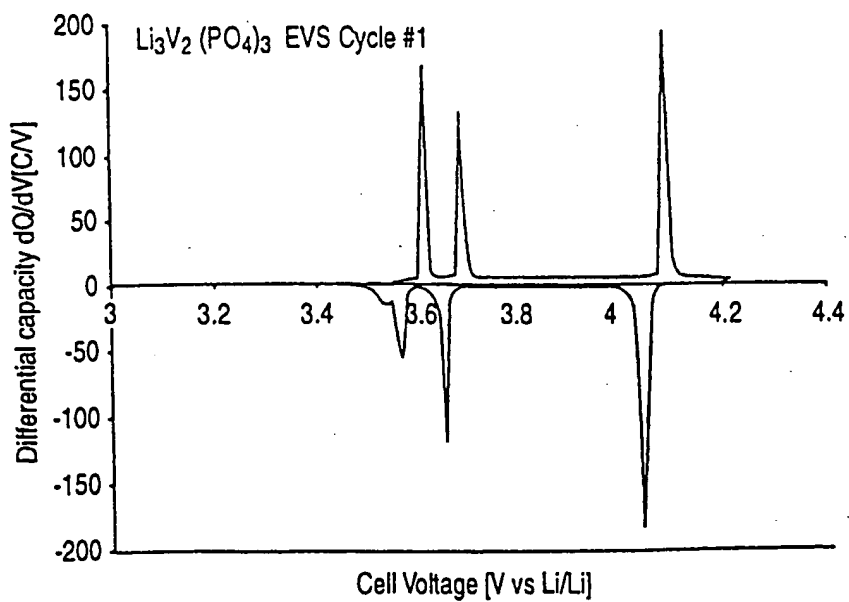
21. The method of claim 20 wherein said at least one metal oxide compound includes V_2O_5 and $Al(OH)_3$; and said reducing atmosphere comprises hydrogen gas.

22. The method of claim 19 wherein said reacting step (b) is conducted by:

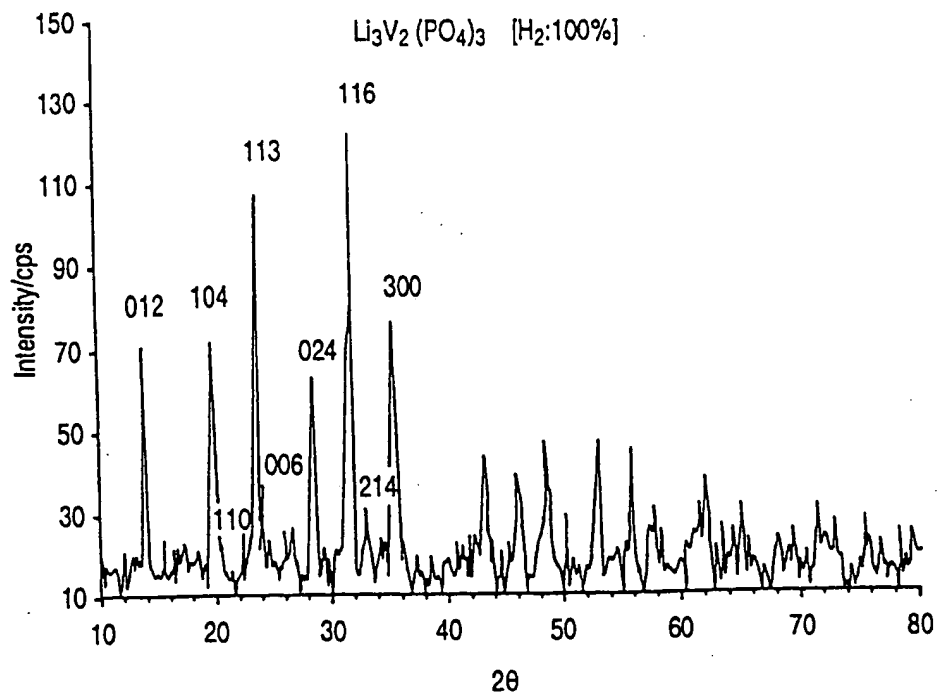
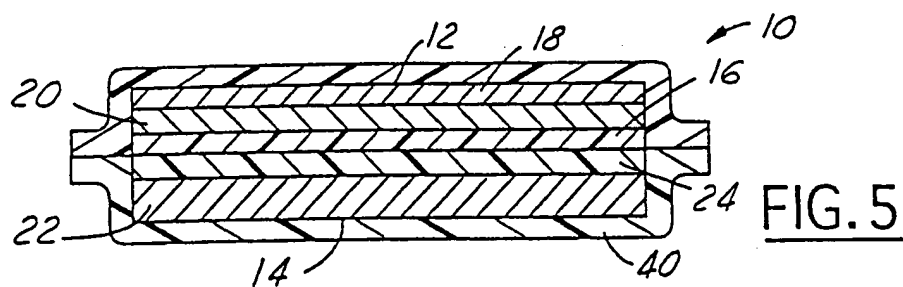
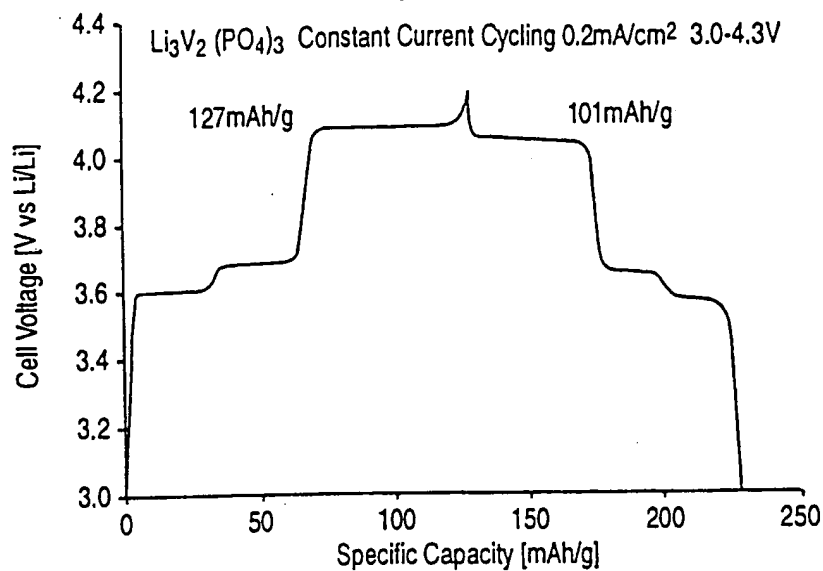
- (i) heating to a first temperature sufficient to decompose at least one of said lithium compound and said phosphate salt compound; and then
- (ii) heating to a second temperature sufficient to form said product and less than the decomposition temperature of said product.

23. The method of claim 22 wherein said first temperature is in a range of about 550°C to about 750°C and said second temperature is in a range of about 800°C to about 1000°C.

24. The method of claim 22 wherein after step (b) (ii), said product is ground, and steps (b) (i) and (b) (ii) are repeated in sequence.

FIG. 1FIG. 2

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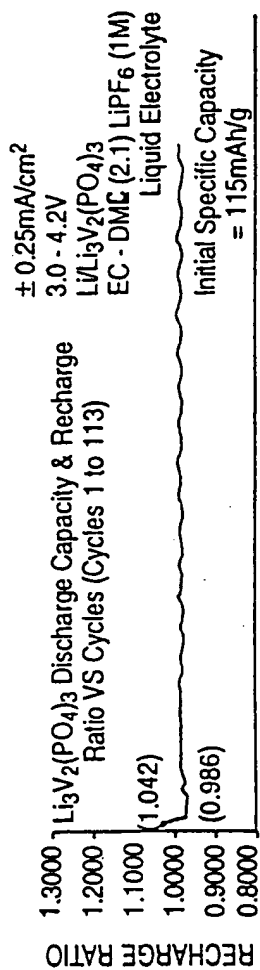


FIG. 4A

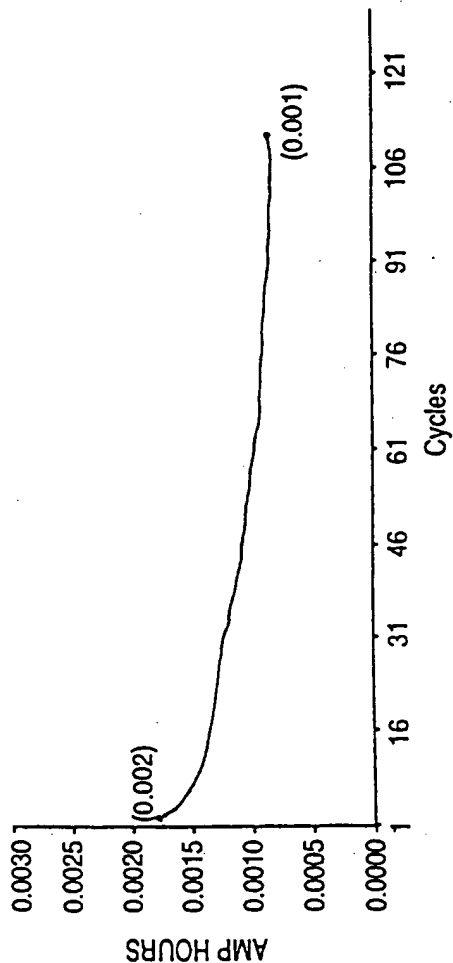
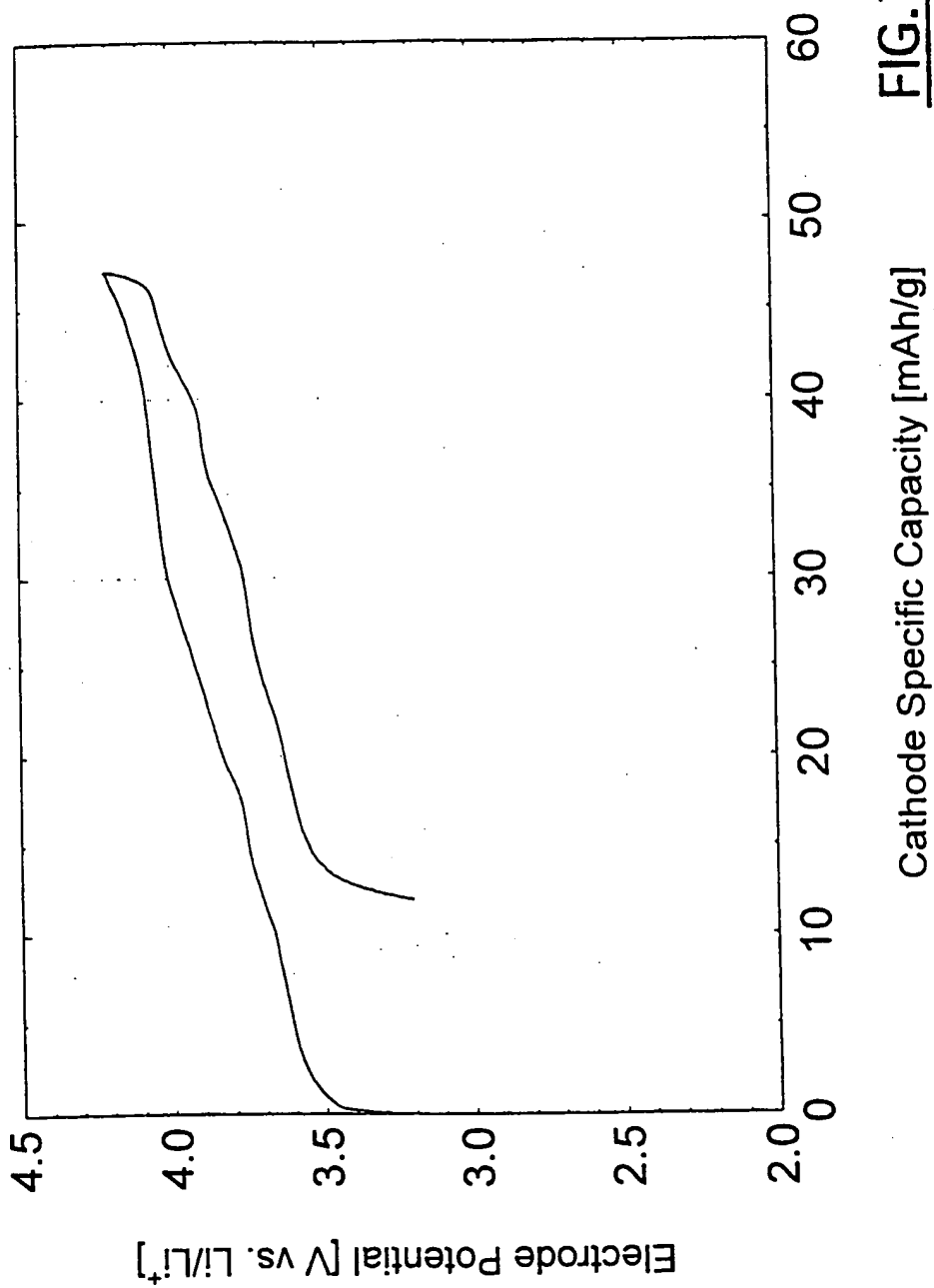


FIG. 4B

Electrochemical Voltage Spectroscopy
Cell#502581 $\text{Li}_3\text{AlV}(\text{PO}_4)_3$ vs. Li



Electrochemical Voltage Spectroscopy
Cell#502581 $\text{Li}_3\text{AlV}(\text{PO}_4)_3$ vs. Li

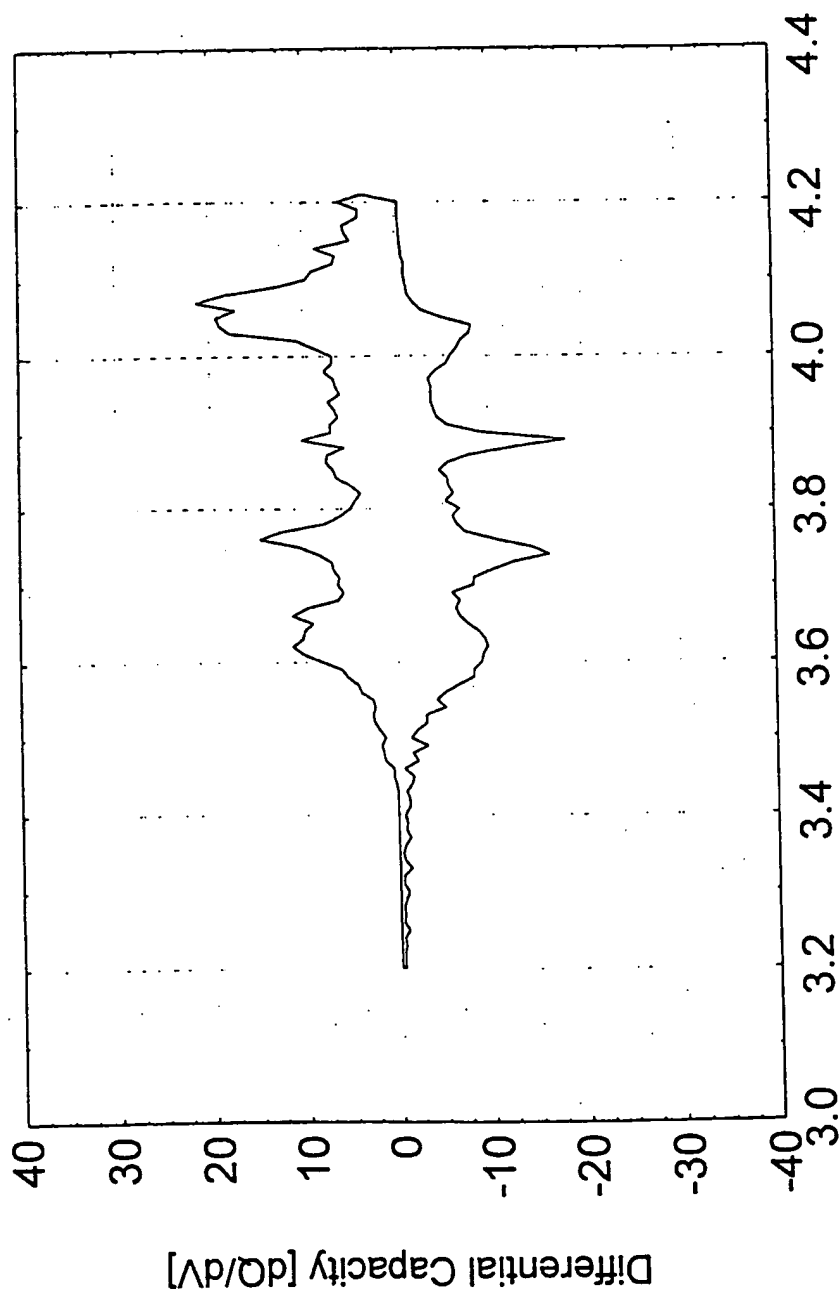


FIG. 8
Electrode Potential [V vs Li/Li⁺]

Cell#502577 Li/Li₃AlV(PO₄)₃
Cycle#1 ±0.05 mA/cm² 3.0-4.5 V

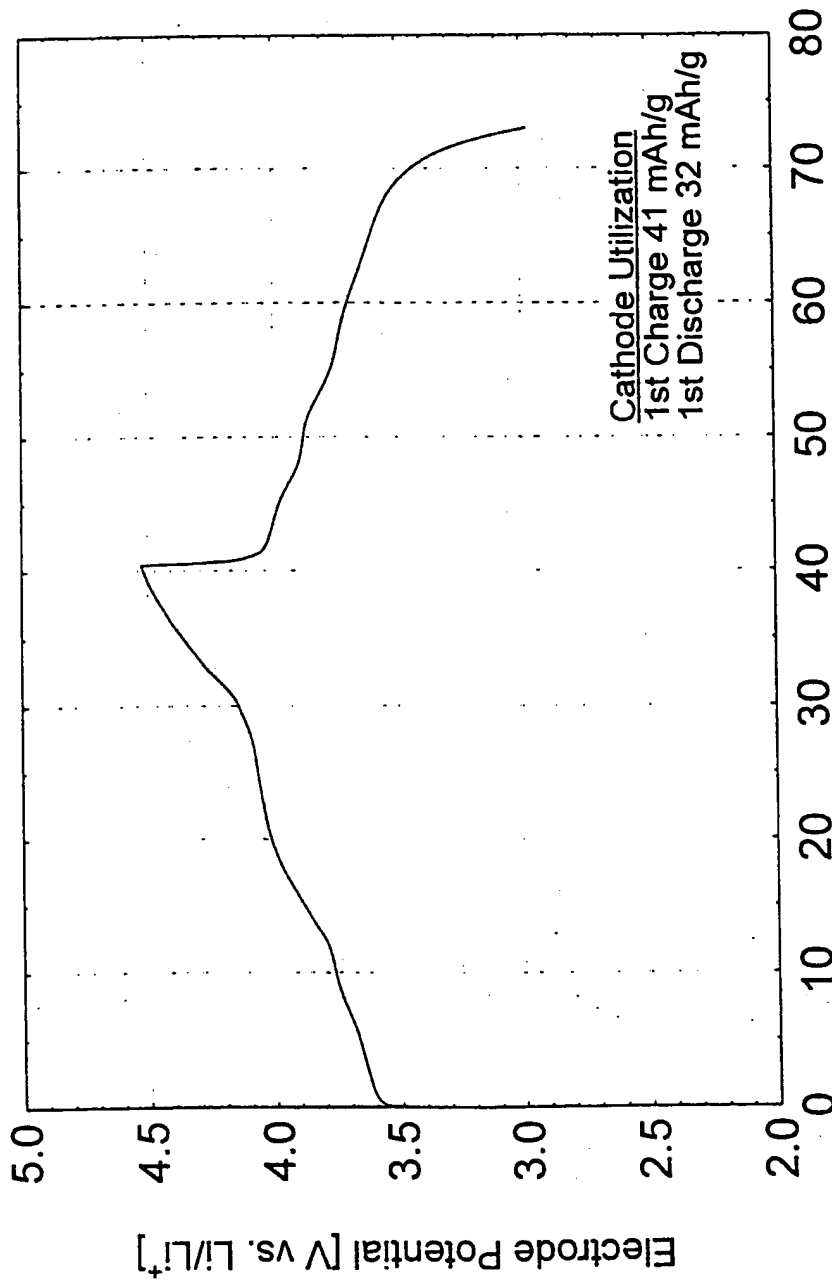


FIG. 9
Cumulative Cathode Specific Capacity [mAh/g]

Cell#502577 Li/Li₃AlV(PO₄)₃
±0.05 mA/cm² 3.0 - 4.5 V

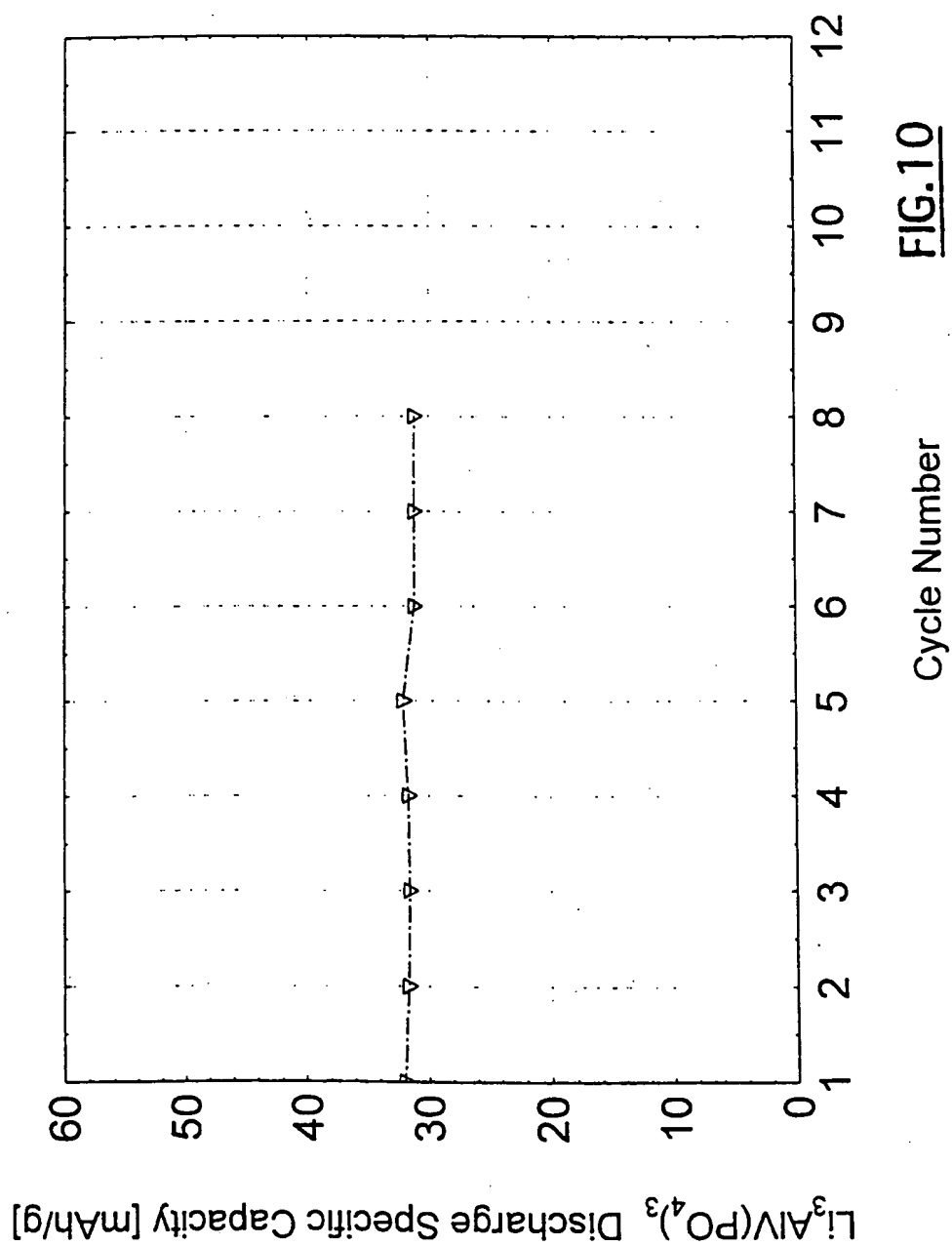
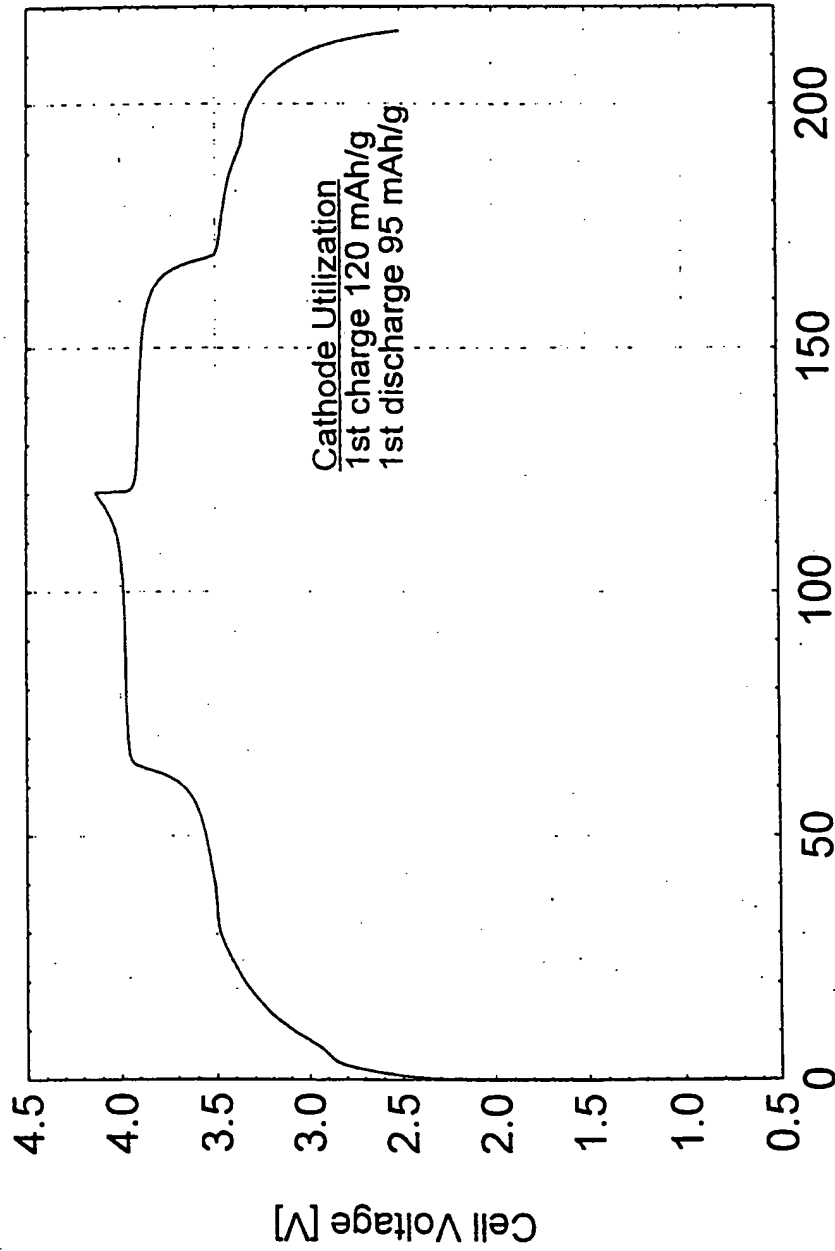


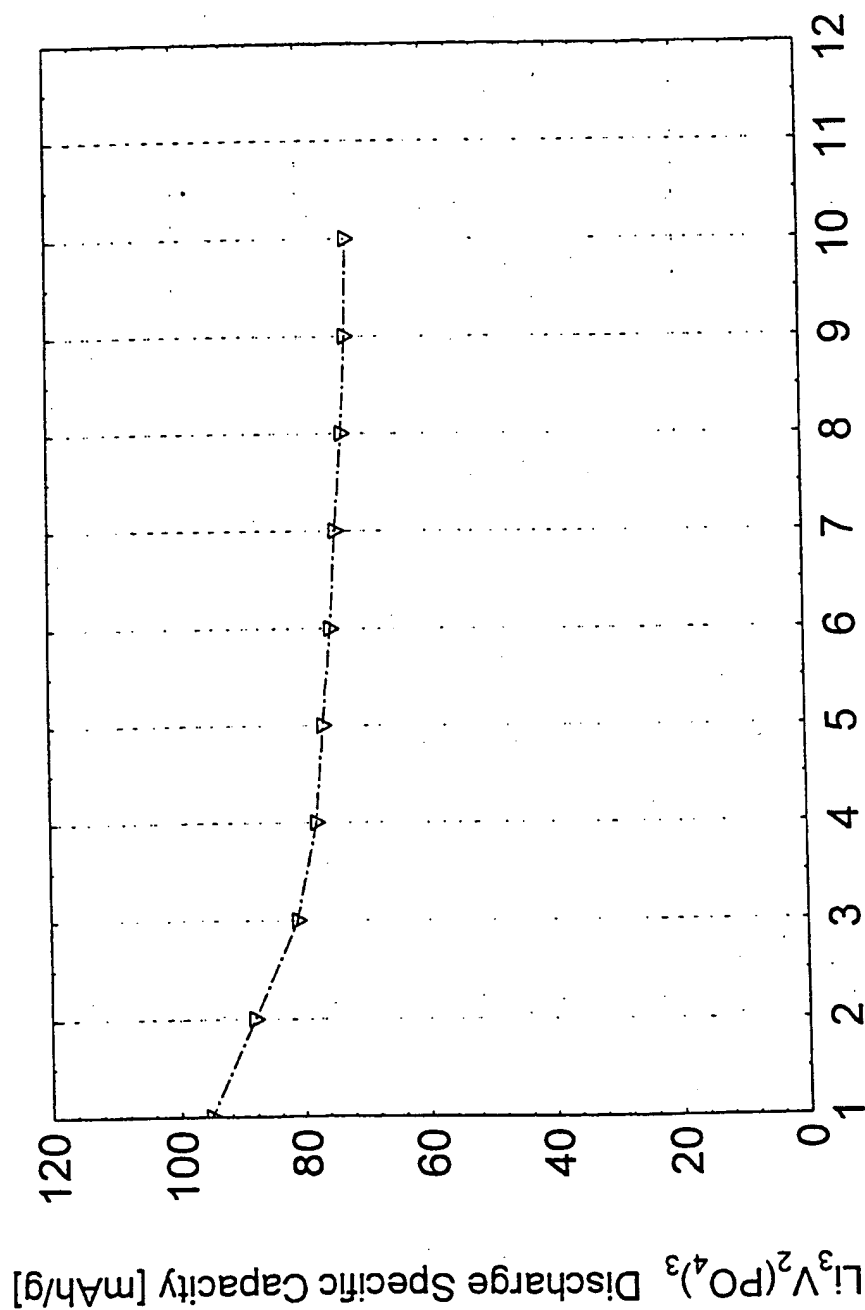
FIG.10

Cell#502582 MCMB2528/Li₃V₂(PO₄)₃
Cycle#1 ±0.2 mA/cm² 2.5 - 4.1 V



Cumulative Cathode Specific Capacity [mAh/g] **FIG. 11**

Cell#502582 MCMB2528/Li₃V₂(PO₄)₃
±0.2 mA/cm² 2.5 - 4.1 V



Cycle Number **FIG.12**

Electrochemical Voltage Spectroscopy
Cell#502653 $\text{Li}_3\text{AlV}(\text{PO}_4)_3$ (Prepared Under H_2 Ambient) vs. Li

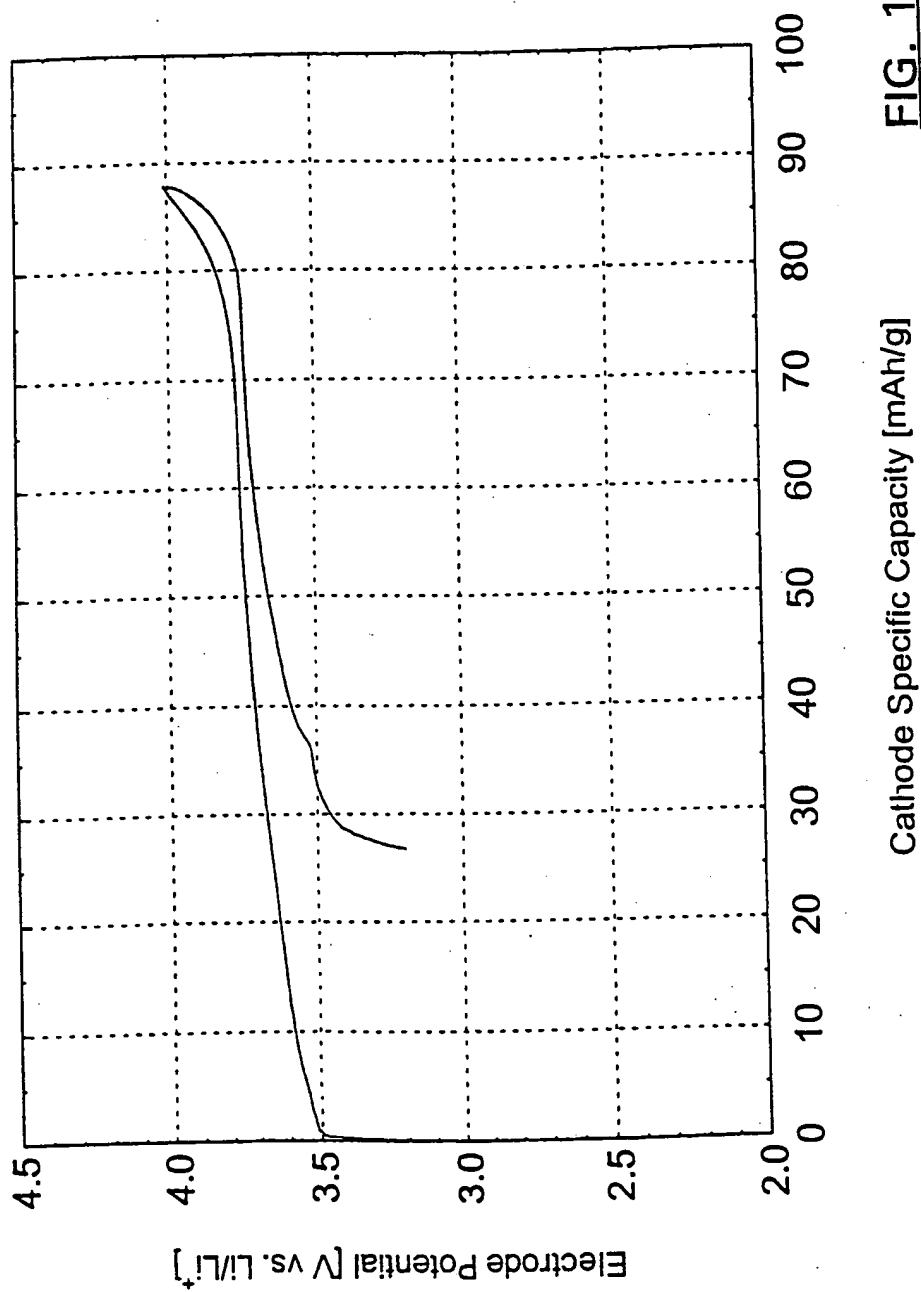


FIG. 13

Electrochemical Voltage Spectroscopy
Cell#502653 $\text{Li}_3\text{AlV}(\text{PO}_4)_3$ (Prepared Under H_2 Ambient) vs. Li

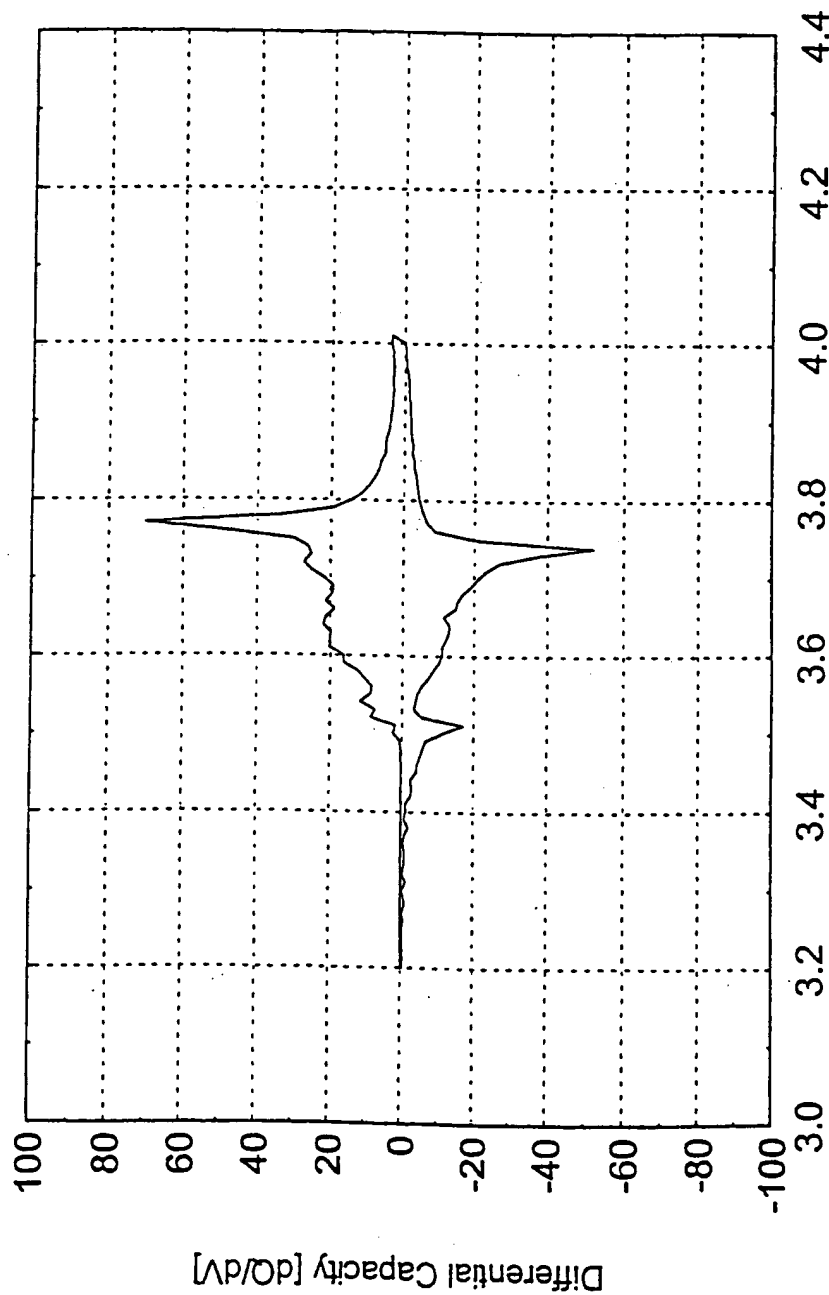


FIG. 14
Electrode Potential [V vs Li/Li⁺]

Cell#502650 $\text{Li/Li}_3\text{AlV}(\text{PO}_4)_3$ Prepared Under H_2 Ambient
Cycle#1 $\pm 0.05 \text{ mA/cm}^2$ 3.0-4.2 V

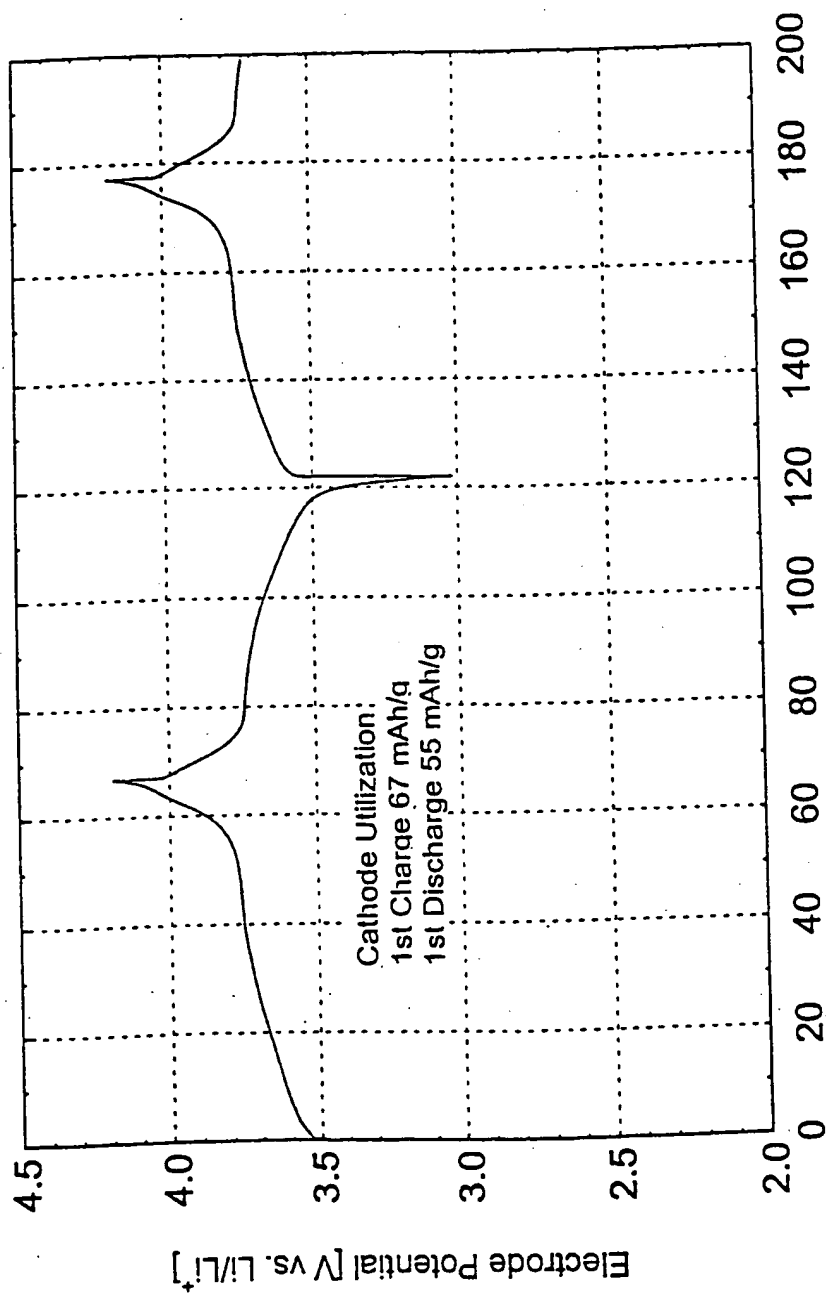


FIG. 15
Cumulative Cathode Specific Capacity [mAh/g]

INTERNATIONAL SEARCH REPORT

International Application No
PCT/US 99/23074

A. CLASSIFICATION OF SUBJECT MATTER

IPC 7 H01M4/58 H01M10/40 C01B25/45

According to International Patent Classification (IPC) or to both national classification and IPC

B. FIELDS SEARCHED

Minimum documentation searched (classification system followed by classification symbols)

IPC 7 H01M C01B

Documentation searched other than minimum documentation to the extent that such documents are included in the fields searched

Electronic data base consulted during the International search (name of data base and, where practical, search terms used)

C. DOCUMENTS CONSIDERED TO BE RELEVANT

Category *	Citation of document, with indication, where appropriate, of the relevant passages	Relevant to claim No.
X	WO 98 12761 A (SAIDI MOHAMED YAZID ;BARKER JEREMY (US); VALENCE TECHNOLOGY INC (U) 26 March 1998 (1998-03-26) page 5, line 19 - line 20; claims 1,8,9,14; example 1 page 24, line 30 - line 35 page 14, line 31 - line 35 page 16, line 18 -page 17, line 24 page 18, line 5 - line 6	1-24
X	WO 97 40541 A (UNIV TEXAS) 30 October 1997 (1997-10-30) claims 6,8,11; example 1	1-19
A		20,22
	-/-	

☒ Further documents are listed in the continuation of box C.

☒ Patent family members are listed in annex.

* Special categories of cited documents:

- "A" document defining the general state of the art which is not considered to be of particular relevance
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 "O" document referring to an oral disclosure, use, exhibition or other means
 "P" document published prior to the international filing date but later than the priority date claimed

- "T" later document published after the international filing date or priority date and not in conflict with the application but cited to understand the principle or theory underlying the invention
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 "Y" document of particular relevance; the claimed invention cannot be considered to involve an inventive step when the document is combined with one or more other such documents, such combination being obvious to a person skilled in the art
 "&" document member of the same patent family

Date of the actual completion of the international search

16 February 2000

Date of mailing of the international search report

24/02/2000

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Andrews, M

INTERNATIONAL SEARCH REPORT

International Application No

PCT/US 99/23074

C.(Continuation) DOCUMENTS CONSIDERED TO BE RELEVANT

Category *	Citation of document, with indication, where appropriate, of the relevant passages	Relevant to claim No.
X	DELMAS C ET AL: "THE NASICON-TYPE TITANIUM PHOSPHATES $\text{ATI}_2(\text{PO}_4)_3$ (A=LI, NA) AS ELECTRODE MATERIALS" SOLID STATE IONICS, NL, NORTH HOLLAND PUB. COMPANY. AMSTERDAM, vol. 28 - 30, no. PART 01, 1 September 1988 (1988-09-01), pages 419-423, XP002048302 ISSN: 0167-2738 experimental, page 420	1,3-5, 8-10,13, 16-19, 22-24
X	DATABASE INSPEC 'Online! INSTITUTE OF ELECTRICAL ENGINEERS, STEVENAGE, GB PADHI A K ET AL: "Mapping of transition metal redox energies in phosphates with NASICON structure by lithium intercalation" Database accession no. 5693819 XP002048304 abstract & JOURNAL OF THE ELECTROCHEMICAL SOCIETY, AUG. 1997, ELECTROCHEM. SOC, USA, vol. 144, no. 8, pages 2581-2586, ISSN: 0013-4651	1-7, 9-15,18

INTERNATIONAL SEARCH REPORT

International application No.

PCT/US 99/ 23074

Box I Observations where certain claims were found unsearchable (Continuation of item 1 of first sheet)

This International Search Report has not been established in respect of certain claims under Article 17(2)(a) for the following reasons:

1. ☐ Claims Nos.:
because they relate to subject matter not required to be searched by this Authority, namely:
2. ☐ Claims Nos.:
because they relate to parts of the International Application that do not comply with the prescribed requirements to such an extent that no meaningful International Search can be carried out, specifically:
3. ☐ Claims Nos.:
because they are dependent claims and are not drafted in accordance with the second and third sentences of Rule 6.4(a).

Box II Observations where unity of invention is lacking (Continuation of item 2 of first sheet)

This International Searching Authority found multiple inventions in this International application, as follows:

SEE ADDITIONAL SHEET

1. ☐ As all required additional search fees were timely paid by the applicant, this International Search Report covers all searchable claims.
2. ☒ As all searchable claims could be searched without effort justifying an additional fee, this Authority did not invite payment of any additional fee.
3. ☐ As only some of the required additional search fees were timely paid by the applicant, this International Search Report covers only those claims for which fees were paid, specifically claims Nos.:
4. ☐ No required additional search fees were timely paid by the applicant. Consequently, this International Search Report is restricted to the invention first mentioned in the claims; it is covered by claims Nos.:

Remark on Protest

- ☐ The additional search fees were accompanied by the applicant's protest.
- ☐ No protest accompanied the payment of additional search fees.

INTERNATIONAL SEARCH REPORT

Information on patent family members

International Application No

PCT/US 99/23074

Patent document cited in search report	Publication date	Patent family member(s)	Publication date
WO 9812761 A	26-03-1998	US 5871866 A AU 4410297 A EP 0931361 A	16-02-1999 14-04-1998 28-07-1999
WO 9740541 A	30-10-1997	EP 0904607 A US 5910382 A	31-03-1999 08-06-1999